**Date Distributed:** 



THE NATIONAL BOARD

OF BOILER AND PRESSURE VESSEL INSPECTORS

# NATIONAL BOARD SUBCOMMITTEE PRESSURE RELIEF DEVICES

AGENDA

Meeting of July 15, 2020 Louisville, KY

The National Board of Boiler & Pressure Vessel Inspectors 1055 Crupper Avenue Columbus, Ohio 43229-1183 Phone: (614)888-8320 FAX: (614)847-1828

#### 1. Call to Order

8:00 AM

#### 2. Announcements

The National Board will be hosting a reception for all committee members and visitors on Wednesday evening at 5:30pm at the SKY Grand Terrace on the 16<sup>th</sup> floor of The Brown Hotel.

#### 3. Adoption of the Agenda

#### 4. Approval of Minutes

The minutes from the January 2020 SC PRD meeting can be found on the National Board website.

#### 5. Review of the Roster (Attachments Page 1)

#### a. Nominations

#### **b.** Reappointments

- Mr. Kim Beise and Mr. Dan Marek have memberships to the subgroup that are set to expire on July 30, 2020.
- Mr. Raymond McCaffrey's membership to the subcommittee is set to expire on August 30, 2020.

#### c. Resignations

#### 6. Interpretations

Item Number: 20-19	NBIC Location: Part 4, 3.3.3.4 & 4.8.5.4	Attachment page 2
General Description: Purpose of NBIC Part 4, Sec. 4.8.5.4, n) 2) & 3.3.3.4, 1) 2) system review		

Task Group: None Assigned

**Explanation of Need:** There appears to be a difference of opinion among VR & T/O Certificate Holders regarding the intent of the "review of the system in order to maintain the manual current with these rules and the applicable sections of the ASME Code." If I am wrong about my interpretation, I want to know. Thank you.

NOTE: the reference to NBIC in 3.3.3.4, 1) 2) at the end of the sentence should be deleted. It is held over from NB-528 and therefore superfluous.

#### July 2020 Meeting Action:

#### 7. Action Items

Item Number: NB12-0901	NBIC Location: Part 4	Attachment Pages 3-9
General Description: Prepare a guide for repair of tank vents		

**Task Group:** B. Donalson (PM), D. DeMichael, K. Simmons, K. Beise, B. Nutter, J. Little, S. Artrip, B. Pittel

**January 2020 Meeting Action:** This item passed unanimously by a voice vote in SG-PRD. This item will be letter balloted to SC-PRD between meetings.

Item Number: NB14-0602B	NBIC Location: Part 2	No Attachment
General Description: Improve inde	x in Part 2 relating to pressure relief devices	

Task Group: D. Marek (PM), B. Donalson, D. DeMichael

January 2020 Meeting Action: No progress on this item.

Item Number: NB15-0108BNBIC Location: Part 1No AttachmentGeneral Description: Address pressure relief devices in new supplement on high temperature hot water<br/>boilers

Task Group: D. Marek (PM), A. Renaldo, D. McHugh, B. Nutter, A. Cox, D. Schirmer

January 2020 Meeting Action: PM was changed to D. Marek. New task group members were added.

Item Number: NB15-0305NBIC Location: Part 4No AttachmentGeneral Description: Create Guidelines for Installation of Overpressure Protection by System Design.

Task Group: B. Nutter, A. Renaldo, D. Marek (PM), D. DeMichael, J. Wolf

January 2020 Meeting Action: Work continues on this item. Jon Wolf was added to the task group.

Item Number: NB15-0307	NBIC Location: Part 4	No Attachment
General Description: Create Guide	ines for Repair of Pin Devices.	

Task Group: D. McHugh (PM), A. Renaldo, T. Tarbay, R. McCaffrey, J. Simms, C. Beair

January 2020 Meeting Action: Work continues on this item. Charlie Beair was added to the task group.

Item Number: NB15-0308NBIC Location: Part 4No AttachmentGeneral Description: - Create Guidelines for Installation of Pressure Relief Devices for Organic Fluid<br/>Vaporizers.

Task Group: T. Patel (PM), K. Beise, B. Nutter

**January 2020 Meeting Action:** Item will be brought back to SG PRD and held pending resolution with ASME action item.

Item Number: NB15-0315 NBIC Location: Part 4, 2.5.6 and 2.6.6 and Part 1, No Attachment 4.5.6 and 5.3.6

**General Description:** Review isolation Valve Requirements, and reword to allow installation of pressure relief devices in upstream piping.

Task Group: D. DeMichael (PM), B. Nutter, A. Renaldo, D. Marek

January 2020 Meeting Action: Work continues on this item.

# Item Number: NB15-0321NBIC Location: Part 4, 3.2.5 a) and Part 2, 2.5.7 a)AttachmentPages 10-17

General Description: Review testing requirements for in-service testing of pressure relief devices

Task Group: A. Cox, A. Renaldo (PM), D. Marek, S. Irvin, D. DeMichael, B. Nutter, J. Ball

**January 2020 Meeting Action:** Passed SC letter ballot and will be letter balloted to Main Committee following this meeting.

**Update:** The proposal was balloted to Main Committee but failed to pass. The ballot received a few negative votes and comments, which can be seen on Attachment Page XXXX.

Item Number: 17-115NBIC Location: Part 4, Section 2Attachment Pages 18-35General Description: Complete rewrite of Section 2 combining common requirements into a general<br/>requirements section for all pressure relief devices and look at combining with 2.4.3, 2.4.4.

Task Group: A. Renaldo (PM), D. McHugh, D. Marek

**January 2020 Meeting Action:** A draft proposal was presented as a progress report. This item will be letter balloted between meetings.

Update: The item received a few negative comments on the SG letter ballot.

Item Number: 17-119NBIC Location: Part 4, 2.2.5 and Part 1, 2.9.1.4No AttachmentGeneral Description: States pressure setting may exceed 10% range. Clarify by how much.

Task Group: T. Patel (PM), D. Marek

**January 2020 Meeting Action:** It was determined that the same language was in ASME Section I. This item is on hold pending completion of ASME action item.

# Item Number: 17-128NBIC Location: Part 4, 2.4.4.3 and Part 1, 3.9.4.3Attachments<br/>Page 36Control DescriptionNumber 1, 11, 2, 4.1.6.Number 1, 3.9.4.3

General Description: allows Y-base to be used while 2.4.1.6 a) prohibits. This appears to be a conflict.

Task Group: B. Nutter (PM), S. Irvin

**January 2020 Meeting Action:** A motion was made and accepted to accept the attached proposal. After discussion a vote was taken and the motion unanimously passed.

**Update:** This item was balloted to Main Committee. The ballot failed to receive enough approval votes, and received a few negative and abstention votes.

Item Number: 18-73NBIC Location: Part 4, 2.3 and Part 1, S5.7.6Attachment Pages 37-43General Description: Update installation requirements for Thermal Fluid Heaters

Task Group: T. Patel (PM), B. Nutter

**January 2020 Meeting Action:** Item was letter balloted to Main Committee and received two negatives. However negatives were responded to with no revisions to the proposal. Item will be revoted on at Main Committee.

**Update:** A new proposal was balloted to SG PRD and SG Installation. The PRD ballot had several unresolved comments, and the Installation ballot failed to receive enough votes to pass.

Item Number: 18-80	NBIC Location: Part 4, S3.1, S4.1, S6.1	Attachments
		Pages 44-48
General Description: Addition	of a "Scope" section to Part 4, S3.1, S4.1, and S	6.1 to stay consistent

with other sections

Task Group: T. Patel (PM), A. Renaldo, K. Simmons, P. Dhobi

**January 2020 Meeting Action:** A motion was made and accepted to accept the attached proposal. After discussion a vote was taken and the motion unanimously passed.

**Update:** A proposal for this item was balloted to the Main Committee. It did not pass, and has a few unresolved comments.

Item Number: 19-1	NBIC Location: Part 4, 4.8.5.4 &	Attachment Page 49
	4.8.6.1	

General Description: Develop specific content and scope of annual field audits.

Task Group: A. Donaldson (PM), D. Marek, A. Cox, P. Dhobi, M. Brodeur, T. Patel

January 2020 Meeting Action: A proposal will be letter balloted between meetings.

**Update:** A proposal was balloted to SG PRD and received several comments to be addressed by the task group.

Item Number: 19-2	NBIC Location: Part 4, 4.9.1	Attachment
		Page 50

**General Description:** Review and clarify requirements for documented training program for VR and T/O programs.

Task Group: A. Donaldson (PM), A. Cox, B. Donaldson, D. Marek, J. Simms

**January 2020 Meeting Action:** A draft proposal was presented as a progress report. Work continues on this item.

**Update:** This item is currently being balloted to the Subgroup.

Item Number: 19-37 NBIC Location: Part 4, 4.3.1 c) 4) No Attachment

General Description: Origin of Replacement Parts for Pressure Relief Devices

Task Group: A. Cox (PM), T. Patel, P. Dhobi, J. Simms

January 2020 Meeting Action: Work continues on this item.

Item Number: 19-71 NBIC Location: Part 4, 4.9.2 & 4.9.3 No Attachment

General Description: Use of Personnel from another VR Certificate Holder to perform VR Repairs.

Task Group: A. Donaldson (PM), A. Cox, B. Donaldson, D. Marek, J. Simms

January 2020 Meeting Action: A task group was formed to work on this item.

Item Number: 19-83 **NBIC Location: Part 4, Part 1** No Attachment General Description: Address alternate pressure relief valve mounting permitted by ASME CC2887-1.

Task Group: D. Marek (PM), T. Patel, J. Ball

January 2020 Meeting Action: A task group was formed to work on this item

Item Number: 19-85 NBIC Location: Part 4, 2.3.6 j) No Attachment General Description: Thermal fluid heaters with no change of phase are not specifically addressed in 2.3.6 j).

Task Group: T. Patel (PM), B. Nutter

January 2020 Meeting Action: A task group was formed to work on this item.

#### **New Items:**

Item Number: 20-9 NBIC Location: Part 4, 9.1 See Attachment on Cloud General Description: Define "Verify" in the NBIC Glossary

**Subgroup:** Repairs and Alterations

Task Group: N. Carter (PM)

Explanation of Need: Defining "Verify" in the NBIC Part 1, 2, 3, and 4 to align with the definition in NB-263, RCI-1, Rules for Commissioned Inspectors.

#### 8. Presentations

### 9. Future Meetings

January 11<sup>th</sup> – 14<sup>th</sup>, 2021 – New Orleans, LA July 12<sup>th</sup> – 15<sup>th</sup>, 2021 – Cincinnati, OH

# 10. Adjournment

Respectfully Submitted,

Thomas P. Beirne, P.E.

Secretary, NBIC Subgroup Pressure Relief Devices

pc: J. Amato B. Weilgozinski J. Ellis

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# Subcommittee Pressure Relief Devices

Last Name	First Name	Interest Category	Role	Exp. Date	More
Brodeur	Marianne	National Board Certificate Holders	Chair	01/30/2022	<u>Details</u>
Cox	J. Alton	General Interest	Vice Chair	01/30/2022	<u>Details</u>
Beirne	Thomas		Secretary	01/30/2099	<u>Details</u>
Beise	Kim	National Board Certificate Holders	Member	01/30/2023	<u>Details</u>
DeMichael	Denis	Users	Member	08/30/2021	<u>Details</u>
Donaldson	Alfred	Manufacturers	Member	01/30/2023	<u>Details</u>
Donalson	Robert	Manufacturers	Member	08/30/2021	<u>Details</u>
Marek	Daniel	General Interest	Member	01/30/2022	<u>Details</u>
McCaffrey	Raymond	General Interest	Member	08/30/2020	<u>Details</u>
McHugh	David	National Board Certificate Holders	Member	01/30/2023	<u>Details</u>
Nutter	Brandon	National Board Certificate Holders	Member	01/30/2022	<u>Details</u>
Patel	Thakor	Manufacturers	Member	01/30/2022	<u>Details</u>
Renaldo	Adam	Users	Member	01/30/2022	<u>Details</u>
Schirmer	Delton	Authorized Inspection Agencies	Member	01/30/2023	<u>Details</u>
Wolf	Jon	Authorized Inspection Agencies	Member	01/30/2023	<u>Details</u>

# PROPOSED INTERPRETATION

Inquiry No.	20-19
	Alton Cox, JAC Consulting, Inc.
Source	alton@jaltoncox.com
Subject	Purpose of NBIC Part 4, Sec. 4.8.5.4, n) 2) & 3.3.3.4, l) 2) system review
	<b>Background:</b> Based on conversations with those affected by this requirement, it is clear that there is widespread misunderstanding regarding the purpose and content of the review required by the above referenced paragraphs. This appears to include not only VR & T/O Certificate Holders, but NB Consultants and members of SC-PRD as well. We need everyone to have the same understanding of this requirement.
	NOTE: the reference to NBIC in 3.3.3.4, l) 2) at the end of the sentence should be deleted. It is held over from NB-528 and therefore superfluous.
Edition	2019 NBIC; Part 4, 3.3.3.4 l) 2), and 4.8.5.4 n) 2)
Question	Question: Does the "Provisions for a review of the system in order to maintain the manual current with these rules and the applicable sections of the ASME Code" refer to a Documented Review of all the QC Aspects of the VR or T/O Holder's QC Program described in the National Board accepted QC Manual?
Reply	Proposed Reply: Yes. The Review of the VR or T/O Certificate Holder's Quality Program, including all aspects of QC System Implementation, shall be conducted, documented, and any required changes implemented within six months of the receipt of the publication of the new Edition of the ASME Code and/or NBIC.
Committee's Question	
Committee's Reply	
Rationale	

Task Group Item NB12\_0901 Repair guidelines for weight-loaded pressure/vacuum vent type pressure relief valve.

# S4.1 Introduction Scope

- a) It is essential that the repair organization establish basic, specific procedures for the repair <u>of weight loaded ventspressure relief valves</u>. The purpose of these recommended procedures is to provide the repair organization with guidelines for this important aspect of valve repair. It is realized that tthere are many types of valves and conditions under which they are repaired and <u>ref</u>or this reason, the specific items in these recommended procedures <u>these recommended procedures</u> may not apply, or they may be inadequate for each of those types or to the detailed repairs that may be required for each other valve.
- b) Prior to removal, repair, or disassembly of a pressure relief valve ensure that all sources of pressure have been removed.
- <u>c)</u>\_S4.2 contains recommended procedures for the repair of spring-loaded pressure relief valves, and S4.3 contains recommended procedures for the repair of pilot operated types of pressure relief valves, and S4.4 contains recommended procedures for the repair of weight loaded-\_vents. Information on packaging, shipping and transportation is included <u>in as</u> S4.5.

# S4.2 SPRING-LOADED PRESSURE RELIEF VALVES (No change)

# S4.3 PILOT OPERATED PRESSURE RELIEF VALVES (No change)

<del>c)</del>

# S4.4 WEIGHT LOADED VENTS

The procedure<u>s</u> -provided in S4.4 are general guidelines<u>ance</u>, and <u>T</u>the manufacturer's information, <u>when available</u>, when available, should be used for detailed instructions based on the vent type and design.

<u>CAUTION: Weight loaded vents are often exposed to hazardous media. An SDS (safety</u> <u>data sheet) should be provided to the repair organization prior to the commencement of any</u> <u>work. If the vent has been exposed to hazardous media, it should be fully decontaminated prior</u> to inspection and disassembly. If the vent has not been fully decontaminated, safety precautions should be taken to adequately protect repair personnel.

<del>a)</del>—

## <u>a)</u>a) A

- <u>1)</u> <u>A</u>ll <u>external components</u> weight loaded vents should be inspected for exterior damage <u>and</u> or corrosion. Also, the vents should be inspected for signs of leakage from the pressure and or vacuum side of the vent.
- 1)2) b) Inspect inlet and outlet flanges. Confirm nameplate information <u>Record manufacturer's nameplate information</u>, such as model, <del>settings,</del> serial number, <del>a</del><u>set point</u>, flow rate, etc. on the repair traveler. nd other information applicable to the vent type being serviced.
- <u>2)3)</u> Record previous repair nameplate information on the repair traveler.
- b) 2) Pre-Disassembly Test Set pressure check
  - a) WWeight loaded vents should may be tested prior to before disassembly to verify check the initial opening of the pressure and/or vacuum setting. of the vent and Also, the vents should be inspected for signs of leakage from the pressure and/or vacuum port. The test results should be recorded record the test results on the repair traveler.

<u>1)</u>

- a) <u>Disassembly</u> Disassembly
- <u>c)</u>
- 1) Safety practices and equipment applicable to the work being performed should be considered prior to commencing the repair. Each vent should be disassembled to the-\_extent necessary for thorough examination. Measures should be taken to ensure-\_traceability and segregation between pressure and vacuum components of the vent-\_assembly. Safety practices and equipment applicable to the work being performed should be considered prior to starting work.
- <u>1)</u>
- 2) Pressure Side Disassembly (as applicable)
  - a. Secure assembly for removal of internal parts. a. \_\_\_\_\_

b. Remove pressure weather hood and <u>screen</u> or <u>cover</u> as applicable . [DDB1]

<u>b.</u>

- Remove weights from pressure side pallet, and place in appropriate bin to maintain traceability and segregation from vacuum side parts.
   <u>Maintain the order in which the weights are stacked if varying sizes,</u> types and/or thickness of weights are used.
- <u>C.</u>
- d. Remove and disassemble pressure pallet assembly, and place in appropriate-bin to maintain traceability and segregation from vacuum side parts.-
- <u>d.</u>
- e. Remov<u>e</u>al pressure seat if applicable and guiding components.
- 3) Vacuum Side Disassembly (as applicable)
  - a. Secure the vent assembly for removal of internal parts.
  - a.<u>b.</u>Remove vacuum <u>cover</u> and screen as applicable.
  - b.c. Remove weights from vacuum side pallet, and place in appropriate bin<u>to maintain traceability and segregation from</u> pressure<u>side parts</u>.
     <u>Maintain the order in which the weights are stacked if varying sizes</u>, <u>types and/or thickness of weights are used</u>.
  - b.<u>d.</u> Remove and disassemble vacuum pallet assembly, and place in bin<u>to maintain traceability and segregation from pressure side parts</u>.
  - c.<u>e.</u>Remov<u>e</u> al of vacuum seat if applicable and guiding components<u>-on</u> some manufacturer's designs as required.

### b)<u>d)</u>Cleaning

- <u>Care should be exercised to avoid damage to components (i.e. nameplates,</u> <u>seating/sealing surfaces, delicate components, etc.) caused by the cleaning method</u> <u>used.</u>
- 1)2) Cleaning method used for weights is dependent on material of construction.
- d)e) Internal Inspection
  - 1) Vent<u>s</u>eat<u>s</u> and sealing surfaces <u>should be inspected</u> for signs of corrosion, erosion, pitting, scratches, cuts, or other damage that would create a leak path.
  - Main body, guiding components, and all pressure retaining attachments should be inspected for signs of wear, corrosion, erosion, <u>pitting</u>, cracks, or other damage that could affect proper operation.

 Nonmetal components including diaphragms, O-rings, and gaskets <u>should be</u> <u>inspected</u> for <u>holes, tears, signs</u> of abnormal wear, or chemical attacks associated with process conditions.

<del>e)<u>f)</u>Repair</del>

 Seating Surfaces should be lapped to a smooth flat surface. <u>Vent seatsSeating</u> <u>Surfaces should be lapped</u> to ensure they are flat<u>-so that to a smooth flat surface is</u> <u>achieved.</u>

2) Metal and non-metal components that are damaged should be replaced.

# f)g)Assembly

If applicable, before <u>beginning the reassembly process</u>, weigh the pallet assembly including <u>the weights</u> for pressure and/or vacuum setting [DDB3]. <u>The m</u>Manufacturer's weight calculations should be used, and the calculated weight for each setting should be recorded on the repair traveler.

- 1) Vacuum Side Assembly (as applicable)
  - a. Secure the vent assembly for safe assembly of internal parts.
  - b. Install vacuum seat and guide as required.
  - <u>b.</u>

<del>c.</del> Assemble and install <u>the</u>vacuum pallet assembly into <u>the</u>main\_-vent body. <u>c.</u>

- d. Install weights on vacuum side pallet assembly. <u>Stack weights from the largest</u> <u>diameter against the pallet.</u> if applicable.
- <u>d.</u>
- e. Install vacuum side <u>cover</u> cap, and screen if applicable.
- 2) Pressure Side Assembly (as applicable)
  - a. Secure the vent for assembly of internal parts.
  - b. Install pressure seat if applicable and guides.
  - c. Assemble and Install pressure pallet assembly into main body.
  - d. Install weights on pressure pallet assembly<u>. Stack weights from the largest</u> <u>diameter against the pallet</u>, if applicable.
  - e. Install pressure weather hood and <u>screen</u> or <u>cover</u> as applicable.

# <del>g)<u>h)</u>Testing</del>

- 1) General Information
  - a. Test equipment used to perform pressure and/or vacuum testing should be of adequate size to safely secure the vent during testing.

- b. All flow meters and pressure/vacuum test gages used should cover the flow rates, and pressure ranges for <u>the v</u>ents being tested<u>.\_Test equipment</u> should be calibrated and traceable to NIST standards.
- 2) Set Pressure Verification
  - a. After final assembly, mount <u>the</u>vent on test stand.
  - b. To check settings, increase pressure <u>or vacuum</u> on the test stand.
    - 1. <u>The pressure setting</u> shall be the test gauge pressure at which an increase in flow rate no longer increases gauge pressure.
    - 2. <u>The v</u>acuum set<u>ting</u> shall be the test gauge pressure at which an increase in flow rate no longer decreases gauge pressure.
  - c. Pallet assembly weight may need to be adjusted to meet pressure/vacuum setting as required.
  - d. If weight adjustments are made <u>the</u>vent should be retested.
  - e. <u>Record</u> set pressure/vacuum on repair traveler.
- 3) Seat Tightness Verification
  - a. Slowly <u>increase the tank pressure to a</u>-minimum of 75% of vent set pressure.
  - b. While maintaining 75% of set pressure for one minute ensure the test leak rate is in accordance with <u>Table 1</u>. This table applies to seat leakage testing for both pressure and vacuum. If the vent fails to meet leak-rate testing, it must be disassembled and repaired. <u>This table complies with the requirements of API</u> <u>2000.</u>

<del>Valve Size</del>	Test Leak-Rate
<del>mm (in.)</del>	<del>m<sup>3</sup>/h (sefh)</del>
<del>≤ 150 (6)</del>	<del>0.014 (0.5)</del>
<del>200 400 (8 16)</del>	<del>0.142 (5.0)</del>
<del>≻ 400 (16)</del>	<del>0.566 (20)</del>

c. Record leak rates on the repair traveler for both pressure and vacuum as applicable.

Table 1: Test Flow Rate			
<b>Specifications</b>			
<u>Vent Size</u>	Test Leak-Rate		
<u>mm (in.)</u>	<u>m³/h (scfh)</u>		
<u>≤ 150 (6)</u>	<u>0.014 (0.5)</u>		
<u>200 – 400 (8 - 16)</u>	<u>0.142 (5.0)</u>		
<u>&gt; 400 (16)</u>	<u>0.566 (20)</u>		

d.—

#### h)<u>i)</u>Sealing

Tamper proof seals should be used to prevent tampering of external adjustments<u>after</u> the vent has been serviced and tested.

i<u>)j)</u>Repair Nameplate

- 1) Repaired <u>b</u>By (organization performing repair)
- 2) Unique identification number
- 3) Date of <u>r</u>Repair
- 4) Model/Type (if changed)
- 5) Pressure <u>s</u>etting (if applicable)
- <u>6)</u>Vacuum <u>s</u>etting (if applicable)

# <u>\$4.4</u>S4.5 PACKAGING, SHIPPING AND TRANSPORTATION OF PRESSURE RELIEF DEVICES

- a) The improper packaging, shipment, and transport of pressure relief devices can have detrimental effects on device operation. Pressure relief devices should be treated with the same precautions as instrumentation, with care taken to avoid rough handling or contamination prior to installation.
- b) The following practices are recommended <u>for spring loaded pressure relief valves and</u> <u>pilot operated pressure relief valves</u> for Direct Spring and Pilot Operated Valves:
  - Valves should be securely fastened to pallets in the vertical position to avoid side loads on guiding surfaces except threaded and socket-weld valves up to NPS 2 (DN 50) may be securely packaged and cushioned during transport.
  - Valve inlet and outlet connection, drain connections, and bonnet vents should be protected during shipment and storage to avoid internal contamination of the valve. Ensure all covers and/or plugs are removed prior to installation.
  - 3) The valve should not be picked up or carried using the lifting lever. Lifting levers should be wired or secured so they cannot be moved while the valve is being shipped or stored. These wires shall be removed before the valve is placed in service.
  - 4) Pilot valve tubing should be protected during shipment and storage to avoid damage and/or breakage.

- 5) Valves for special services, including but not limited to oxygen, chlorine, and hydrogen peroxide, should be packaged in accordance with the appropriate standards and/or owner procurement requirements.
- c) The following practices are recommended for weight loaded <u>ventventss</u>:
  - <u>1)</u> Vents should be securely fastened to pallets in the vertical position to avoid side loads on guiding surfaces, or otherwise securely packaged and cushioned during transport.
  - 1)2) Weights packaged and shipped separately should be marked or Alabeled as <u>either pressure</u>, or vacuum prior to shipment. These segregated weights should be installed at the time of field installation, paying close attention as to whether they are pressure or vacuum weights.
  - <u>2)3</u>\_All shipping blocks, metal bands,<u>any</u>protective inserts<u></u>, and inlet/outlet protective covers that may be used for shipment must be removed prior to placing the vent in service.

NB15-0321 AMR suggested edits 6-30-2020

Main Committee Ballot comments:

Mr. Rick Sturm: I have voted against this as I believe that in 3.2.4.4 paragraph 11 and 12 as well as where wording is duplicated in 2.5.5.4 the "should's" should be changed to "Shall" i.e. checking for bends/deflections of pins or bars, markings on pins as well as shall be taken out of service. If someone can provide me with why they can remain a should instead of a shall I would appreciate it.

Mr. Donnie LeSage: I had the same thoughts as Mr. Rick Sturm as I was reading the proposal. I agree with his recommendation to change the Shoulds to Shall.

Mr. Venus Newton: You should be providing clearer guidance on what is meant by "periodic" and periodically means. The code needs to be as specific as we can about how often to perform these tests.

Mr. Rob Troutt: I agree with Mr. Rick Sturm, the word "should" needs to be changed to "Shall".

Mr. Bob Wielgoszinski:

Part 4:

- 3.2.4.4g) 13) add the word "to" before prevent in the 2nd line.
- 3.2.5.2c) reference is made to "3.2.6". I could not locate that paragraph. Is the 1 through 6 below 3.2.5.2c) intended to be 3.2.6?
- 3.2.5.4a) although it does not appear to part of this action, the text says that the system "should" be taken out of service if the pin/bar is stuck closed. Should that be changed to "shall"? Why would we have a system running with a dysfunctional PRD?

Part 2: (NOTE THAT THESE ARE MUCH THE SAME COMMENTS AS FOR PART 4 above)

- 2.5.5.4g)13) add the word "to" before prevent in the 2nd line.
- 2.5.7.2 c) I see no requirements of instruction for freedom of motion inspection in 2.5.8. Was the 1 through 6 below intended to be the instruction?
- 2.5.7.4a) although it does not appear to part of this action, the text says that the system "should" be taken out of service if the pin/bar is stuck closed. Should that be changed to "shall"? Why would we have a system running with a dysfunctional PRD?

PART 4

#### 3.2.4.4 RUPTURE DISKSNON-RECLOSING PRESSURE RELIEF DEVICES

g) For rupture disks and other non-reclosing devices, the following additional items should be considered during inspections.

No changes under 3.2.4.4 g)1) through g)10). New text as follows under 3.2.4.4 g)11) through g)14).

<u>11) For non-reclosing PRDs that use pins or bars, those components should be checked for bends/deflection, cracks, or corrosion. Pin deflection may be the results of pin fasteners being overtightened.</u>

12) For non-reclosing PRDs that use pins or bars, the markings on those components should be checked against information on the device nameplate to ensure that they are installed on the correct device. If markings are illegible or missing, the device should be taken out of service and the pin or bar should be replaced with a component specified by the manufacturer. Replacement shall not be performed while the device is pressurized.

13) For non-reclosing PRDs that use pins or bars, check that there is no foreign object present that could interfere with the bar or pin, prevent proper operation of the device, hold the device shut.

<u>14) It is recommended that pins or bars be replaced periodically to prevent unintended failure while in service due to deterioration of the load-bearing component.</u>

# 3.2.5 <u>GENERAL CONSIDERATIONS FOR</u> TESTING AND OPERATIONAL INSPECTION OF PRESSURE RELIEF DEVICES

a) Pressure relief valves shall be tested periodically to ensure that they are free to operate and will operatedevices shall be subject to periodic inspection and/or testing based upon the type of device. in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure, reclosing pressure, where applicable, and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction shall be used to detormine the acceptability of test results.

b) Testing may be accomplished by the owner on the unit where the valve is installed or at a qualified test facility. In many cases, testing on the unit may be impractical, especially if the service fluid is hazardous or toxic. Testing on the unit may involve the bypassing of operating controls and should only be performed

by qualified individuals under carefully controlled conditions. It is recommended that a written procedure be available to conduct this testing.

1) The Inspector should ensure that calibrated equipment has been used to perform this test and the results should be documented by the owner.

2) If the testing <u>was is performed at a test facility, the record of this test should be reviewed to ensure the valve-device</u> meets the requirements of the original code of construction. <u>Valves Devices</u> which have been in toxic, flammable, or other hazardous services shall be carefully decontaminated before being tested. In particular, the closed bonnet of valves in these services may contain fluids that are not easily removed or neutralized. If a test cannot be safely performed, the <u>valve-device</u> shall be disassembled, cleaned, and-decontaminated, repaired, and reset.

3) If a <u>valve\_device</u> has been removed for testing, the inlet and outlet connections should be checked for blockage by product buildup or corrosion.

### 3.2.5.1 TESTING AND OPERATIONAL INSPECTION OF PRESSURE RELIEF VALVES

#### In addition to 3.2.5, the following apply to testing and operational inspection of pressure relief valves.

a) Pressure relief valves shall be tested periodically to ensure that they are free to operate and will operate in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure, reclosing pressure, where applicable, and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction shall be used to determine the acceptability of test results.

b) Valves may be tested using lift assist devices when testing at full pressure may cause damage to the valve being tested, or it is impractical to test at full pressure due to system design considerations. Lift assist devices apply an auxiliary load to the valve spindle or stem, and using the measured inlet pressure, applied load and other valve data allow the set pressure to be calculated. If a lift assist device is

used to determine valve set pressure, the conditions of 4.6.3 shall be met. It should be noted that false set pressure readings may be obtained for valves which are leaking excessively or otherwise damaged.

ec) If valves are not tested on the system using the system fluid, the following test mediums shall be used:

1) High pressure boiler pressure relief valves, high temperature hot-water boiler pressure relief valves, low pressure steam heating boilers: steam;

2) Hot-water heating boiler pressure relief valves: steam, air, or water;

3) Hot water heater temperature and pressure relief valves: air or water;

4) Air and gas service process pressure relief valves: air, nitrogen, or other suitable gas;

5) Liquid service process pressure relief valves: water or other suitable fluid;

6) Process steam service pressure relief valves: steam or air with manufacturer's steam to air correction factor.

Note: Valves being tested after a repair must be tested on steam except as permitted by 4.6.2.

ed) As an alternative to a pressure test, the valve may be checked by the owner for freedom of operation by activating the test or "try" lever (manual check). For high pressure boiler and process valves, this test should be performed only at a pressure greater than 75% of the stamped set pressure of the valve or the lifting device may be damaged. This test will only indicate that the valve is free to operate and does not provide any information on the actual set pressure. All manual checks should be performed with some pressure under the valve in order to flush out debris from the seat that could cause leakage.

**Note**: The manual check at 75% or higher is based on lift lever design requirements for ASME Section I and VIII valves. Code design requirements for lifting levers for Section IV valves require that the valve be capable of being lifted without pressure.

fe) Systems with multiple valves will require the lower set valves to be held closed to permit the higher set valves to be tested. A test clamp or "gag" should be used for this purpose. The spring compression screw shall not be tightened. It is recommended that the test clamps be applied in accordance with the valve manufacturer's instructions when the valve is at or near the test temperature, and be applied hand tight only to avoid damage to the valve stem or spindle.

<u>gf</u>) Upon completion of set pressure testing, all pressure relief valve gags shall be removed. <u>Any stop</u> valves used to isolate lower set pressure relief devices shall be reopened (and locked, if applicable).

#### 3.2.5.2 TESTING AND OPERATIONAL INSPECTION OF NON-RECLOSING PRESSURE RELIEF DEVICES WITH PINS OR BARS

In addition to 3.2.5, the following apply to testing and operational inspection of non-reclosing PRDs with pins or bars.

a) Periodic set point testing is not required since pins or bars are single use.

b) Periodic inspection shall be per 3.2.4.4.

c) Non-reclosing PRDs shall be periodically inspected by the owner for freedom of motion. Freedom of motion inspection frequency shall be per 3.2.6.

<u>1) Remove pressure from the PRD, or remove the PRD from service, prior to performing this check.</u>

2) Remove the pin or bar.

3) Manually exercise the sealing mechanism to ensure it is capable of its full range of motion.

<u>4) Reinstall the pin or bar or replace with new. Replacement pin or bar shall be per manufacturer recommendation.</u>

5) Restore pressure to the PRD.

6) The PRD should be checked for seat leakage following restoration of pressure.

d) The owner may elect to have a non-reclosing PRD tested periodically in order to determine service life of the device. Such tests should ensure that the PRD is free to operate and will operate in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction should be used to determine the acceptability of test results.

## **3.2.5.3 TESTING AND OPERATIONAL INSPECTION OF RUPTURE DISKS**

In addition to 3.2.5, the following apply to testing and operational inspection of rupture disks.

a) Periodic testing of rupture disks is not required

b) Rupture disks shall be subject to periodic inspection per 3.2.4.4.

c) The owner may elect to have a rupture disks tested periodically in order to determine service life. Such tests should ensure that the disk is free to operate inside its holder and will operate in accordance with the requirements of the original code of construction. Testing should include an evaluation of leakage through the disk (e.g. due to cracks or porosity), followed by device opening or burst pressure at rated temperature. Tolerances specified for these operating requirements in the original code of construction should be used to determine the acceptability of test results.

d) If PRDs are not tested on the system using the system fluid, the following test mediums shall be used:

1) Air and gas service PRDs: air, nitrogen, or other suitable gas;

2) Liquid service PRDs: water or other suitable fluid.

#### 3.2.5.1 <u>4</u>CORRECTIVE ACTION

a) If a valve-pressure relief valve or a non-reclosing PRD that is actuated by a pin or bar is found to be stuck closed, the system should immediately be taken out of service until the condition can be corrected, unless special provisions have been made to operate on a temporary basis (such as additional relief capacity provided by another valve.) The owner shall be notified and corrective action such

as repairing or replacing the inoperable valve device shall be taken.

b) If a pressure relief device leaks, the owner shall be notified and decide what corrective action (if any) will be taken.

#### PART 2

### 2.5.5.4 RUPTURE DISKSNON-RECLOSING PRESSURE RELIEF DEVICES

g) For rupture disks and other non-reclosing devices, the following additional items should be considered during inspections.

No changes under 2.5.5.4 g)1) through g)10). New text as follows under 2.5.5.4 g)11) through g)14).

<u>11) For non-reclosing PRDs that use pins or bars, those components should be checked for bends/deflection, cracks, or corrosion. Pin deflection may be the results of pin fasteners being overtightened.</u>

12) For non-reclosing PRDs that use pins or bars, the markings on those components should be checked against information on the device nameplate to ensure that they are installed on the correct device. If markings are illegible or missing, the device should be taken out of service and the pin or bar should be replaced with a component specified by the manufacturer. Replacement shall not be performed while the device is pressurized.

<u>13) For non-reclosing PRDs that use pins or bars, check that there is no foreign object present that could interfere with the bar or pin, prevent proper operation of the device, hold the device shut.</u>

<u>14) It is recommended that pins or bars be replaced periodically to prevent unintended failure while in service due to deterioration of the load-bearing component.</u>

# 2.5.7 <u>GENERAL CONSIDERATIONS FOR</u> TESTING AND OPERATIONAL INSPECTION OF PRESSURE RELIEF DEVICES

a) Pressure relief valves shall be tested periodically to ensure that they are free to operate and will operatedevices shall be subject to periodic inspection and/or testing based upon the type of device. in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure, reclosing pressure, where applicable, and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction shall be used to determine the acceptability of test results.

b) Testing may be accomplished by the owner on the unit where the valve is installed or at a qualified test facility. In many cases, testing on the unit may be impractical, especially if the service fluid is hazardous or toxic. Testing on the unit may involve the bypassing of operating controls and should only be performed

by qualified individuals under carefully controlled conditions. It is recommended that a written procedure be available to conduct this testing.

1) The Inspector should ensure that calibrated equipment has been used to perform this test and the results should be documented by the owner.

2) If the testing <u>was is performed at a test facility, the record of this test should be reviewed to ensure the valve-device</u> meets the requirements of the original code of construction. <u>Valves Devices</u> which have been in toxic, flammable, or other hazardous services shall be carefully decontaminated before being tested. In particular, the closed bonnet of valves in these services may contain fluids that are not easily removed or neutralized. If a test cannot be safely performed, the <u>valve-device</u> shall be disassembled, cleaned, and-decontaminated, repaired, and reset.

3) If a <u>valve device</u> has been removed for testing, the inlet and outlet connections should be checked for blockage by product buildup or corrosion.

## 2.5.7.1 TESTING AND OPERATIONAL INSPECTION OF PRESSURE RELIEF VALVES

#### In addition to 2.5.7, the following apply to testing and operational inspection of pressure relief valves.

a) Pressure relief valves shall be tested periodically to ensure that they are free to operate and will operate in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure, reclosing pressure, where applicable, and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction shall be used to determine the acceptability of test results.

b) Valves may be tested using lift assist devices when testing at full pressure may cause damage to the valve being tested, or it is impractical to test at full pressure due to system design considerations. Lift assist devices apply an auxiliary load to the valve spindle or stem, and using the measured inlet pressure, applied load and other valve data allow the set pressure to be calculated. If a lift assist device is used to determine valve set pressure, the conditions of 4.6.3 shall be met. It should be noted that false set pressure readings may be obtained for valves which are leaking excessively or otherwise damaged.

ec) If valves are not tested on the system using the system fluid, the following test mediums shall be used:

1) High pressure boiler pressure relief valves, high temperature hot-water boiler pressure relief valves, low pressure steam heating boilers: steam;

2) Hot-water heating boiler pressure relief valves: steam, air, or water;

3) Hot water heater temperature and pressure relief valves: air or water;

4) Air and gas service process pressure relief valves: air, nitrogen, or other suitable gas;

5) Liquid service process pressure relief valves: water or other suitable fluid;

6) Process steam service pressure relief valves: steam or air with manufacturer's steam to air correction factor.

Note: Valves being tested after a repair must be tested on steam except as permitted by 4.6.2.

ed) As an alternative to a pressure test, the valve may be checked by the owner for freedom of operation by activating the test or "try" lever (manual check). For high pressure boiler and process valves, this test should be performed only at a pressure greater than 75% of the stamped set pressure of the valve or the lifting device may be damaged. This test will only indicate that the valve is free to operate and does not provide any information on the actual set pressure. All manual checks should be performed with some pressure under the valve in order to flush out debris from the seat that could cause leakage.

**Note**: The manual check at 75% or higher is based on lift lever design requirements for ASME Section I and VIII valves. Code design requirements for lifting levers for Section IV valves require that the valve be capable of being lifted without pressure.

fe) Systems with multiple valves will require the lower set valves to be held closed to permit the higher set valves to be tested. A test clamp or "gag" should be used for this purpose. The spring compression screw shall not be tightened. It is recommended that the test clamps be applied in accordance with the valve manufacturer's instructions when the valve is at or near the test temperature, and be applied hand tight only to avoid damage to the valve stem or spindle.

<u>gf</u>) Upon completion of set pressure testing, all pressure relief valve gags shall be removed. <u>Any stop</u> valves used to isolate lower set pressure relief devices shall be reopened (and locked, if applicable).

#### 2.5.7.2 TESTING AND OPERATIONAL INSPECTION OF NON-RECLOSING PRESSURE RELIEF DEVICES WITH PINS OR BARS

In addition to 2.5.7, the following apply to testing and operational inspection of non-reclosing PRDs with pins or bars.

a) Periodic set point testing is not required since pins or bars are single use.

b) Periodic inspection shall be per 2.5.5.4.

<u>c) Non-reclosing PRDs shall be periodically inspected by the owner for freedom of motion. Freedom of motion inspection frequency shall be per 2.5.8.</u>

<u>1) Remove pressure from the PRD, or remove the PRD from service, prior to performing this check.</u>

2) Remove the pin or bar.

3) Manually exercise the sealing mechanism to ensure it is capable of its full range of motion.

<u>4) Reinstall the pin or bar or replace with new. Replacement pin or bar shall be per manufacturer recommendation.</u>

5) Restore pressure to the PRD.

6) The PRD should be checked for seat leakage following restoration of pressure.

d) The owner may elect to have a non-reclosing PRD tested periodically in order to determine service life of the device. Such tests should ensure that the PRD is free to operate and will operate in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction should be used to determine the acceptability of test results.

### 2.5.7.3 TESTING AND OPERATIONAL INSPECTION OF RUPTURE DISKS

In addition to 2.5.7, the following apply to testing and operational inspection of rupture disks.

a) Periodic testing of rupture disks is not required

b) Rupture disks shall be subject to periodic inspection per 2.5.5.4.

c) The owner may elect to have a rupture disks tested periodically in order to determine service life. Such tests should ensure that the disk is free to operate inside its holder and will operate in accordance with the requirements of the original code of construction. Testing should include an evaluation of leakage through the disk (e.g. due to cracks or porosity), followed by device opening or burst pressure at rated temperature. Tolerances specified for these operating requirements in the original code of construction should be used to determine the acceptability of test results.

d) If PRDs are not tested on the system using the system fluid, the following test mediums shall be used:

1) Air and gas service PRDs: air, nitrogen, or other suitable gas;

2) Liquid service PRDs: water or other suitable fluid.

## 2.5.7.1 4 CORRECTIVE ACTION

a) If a valve pressure relief valve or a non-reclosing PRD that is actuated by a pin or bar is found to be stuck closed, the system should immediately be taken out of service until the condition can be corrected, unless special provisions have been made to operate on a temporary basis (such as additional relief capacity provided by another valve.) The owner shall be notified and corrective action such

as repairing or replacing the inoperable valve <u>device</u> shall be taken.

b) If a pressure relief device leaks, the owner shall be notified and decide what corrective action (if any) will be taken.

# PART 4, SECTION 2 PRESSURE RELIEF DEVICES — INSTALLATION OF PRESSURE RELIEF DEVICES

#### 2.1 SCOPE

NBIC Part 4 Section 2 provides requirements for the installation of pressure relief devices on power boilers,

steam heating boilers, hot-water heating boilers, hot-water supply boilers, potable water heaters, pressure vessels and piping.

The correct selection of appropriate pressure relief devices (PRDs) and the proper installation of those devices

are critical to the safe operation of pressure retaining items. Following are requirements for the installation of

pressure relief devices for protection of different types of pressurized equipment. See NBIC Part 1 for general

installation requirements.

2.1.1 GENERAL REQUIREMENTS FOR INSTALLATION OF PRESSURE RELIEF DEVICES

#### 2.1.1.1 RELIEF DEVICE DESIGN & NUMBER

a) Pressure retaining items shall be equipped with one or more pressure relief devices unless the option for overpressure protection by system design is utilized (when permitted by the Jurisdiction and the original code of construction). Multiple isolatable chambers, or system portions with different maximum allowable working pressures, shall have their own pressure relief device(s) to protect the chambers under the most severe coincident conditions.

b) A pressure relief device and its associated piping shall be safely supported. Design of supports, foundations, and settings shall consider vibration (including seismic where necessary), movement (including thermal movement), and loadings (including reaction forces) in accordance with jurisdictional requirements, manufacturer's recommendations, and/or other industry standards, as applicable. Piping shall be supported in a manner that avoids placing undue stress on the body of the pressure relief device. c) Pressure relief devices shall be manufactured in accordance with a national or international standard. d) Pressure relief devices shall have their capacity certified by the National Board unless otherwise permitted by the original code of construction

e) Pressure relief devices shall be selected (i.e., material, pressure, etc.) and installed such that their proper functioning will not be hindered by the nature of the system's contents.

f) When a pressure relief valve is exposed to outdoor elements that may affect operation of the valve, the valve may be shielded with a cover. The cover shall be properly vented and arranged to permit servicing and normal operation of the valve.

g) <u>A non-reclosing device (rupture disk) may be installed on the inlet and/or outlet of a pressure relief</u> valve when permitted by the original code of construction. The reduction in capacity due to installation of the non-reclosing device shall be determined by use of a National Board certified Combination Capacity Factor (CCF).

For rupture disks, if a certified combination capacity factor is not available, the capacity of the pressure relief valve shall be multiplied by 0.9 and this value used as the capacity of the combination installation. thereduction in capacity due to installation of the non reclosing device shall be determined in accordance with the code of construction by use of a National Board certified Combination Capacity Factor (CCF). For rupture disks, if a certified combination capacity factor is not available, the capacity of the pressure relief valve shall be multiplied by 0.9 and this value used as the capacity of the pressure of the combination installation.

<u>h) The effect of inlet pressure drop and discharge back pressure on relief device capacity shall be</u> considered in the system design and relief device selection.

i) Twin pressure relief valves made by placing individual valves on Y-bases or duplex valves having two valves in the same body shall be of equal size.

j) The owner shall document the basis for selection of the pressure relief devices used, including capacity, and have such calculations available for review by the Jurisdiction.

k) Pressure relief devices shall be in accordance with the code of construction and

designed for liquid, vapor, or combination service as required for the specific installation, service fluids, and overpressure conditions.

#### 2.1.1.2 DESIGN OF RELIEF DEVICE INLET LINES

a) Pressure relief devices shall be installed directly on, or as close as possible to, the pressure retaining item, and be installed so they are accessible for inspection, repair, or replacement. The opening in the pressure retaining item shall provide unobstructed flow to the pressure relief device. If multiple relief valves are installed on the same connection to the pressure retaining item, the opening shall have a cross-sectional area not less than the combined areas of inlet connections of all the pressure relief valves with which it connects.

b) Inlet lines shall be as short and straight as possible. Inlet lines shall be properly supported in accordance with 2.1.1.1 b).

c) The opening through all pipes and fittings between a pressure retaining item and its pressure relief device shall have at least the area of the pressure relief device inlet. The characteristics of this upstream system shall be such that the pressure drop will not reduce the relieving capacity below that required or adversely affect the operation of the pressure relief device.

d) When a pressure retaining item is fitted with one or more pressure relief devices on one connection, the inlet cross-sectional area of this connection shall be sized either to avoid restricting flow to the pressure relief devices or to have a cross sectional area not less than the combined areas of inlet connections of all the pressure relief devices with which it connects.

e) When a Y-base is used, the inlet area shall be not less than the combined outlet areas.

f) Inlets to pressure relief devices intended for use in compressible fluid or steam service shall be

connected to the vessel in the vapor space above any contained liquid or in the piping system connected to the vapor space.

g) Pressure relief devices intended for use in liquid service shall be connected below the normal liquid line. The liquid level during upset conditions shall be considered.

h) Unless permitted by the code of construction, the Jurisdiction, and the requirements specific to the type of pressure retaining item found in Section 2, there shall be no intervening stop valve or changeover valve between the pressure retaining item and its pressure relief device(s),

i) Where an intervening stop valve is permitted and used, it shall comply with 2.1.1.4.

i) Where a changeover valve is permitted and used, it shall comply with 2.1.1.5.

#### 2.1.1.3 DESIGN OF RELIEF DEVICE DISCHARGE LINES

a) Discharge lines shall be as short and straight as possible. Discharge lines shall be properly supported in accordance with 2.1.1.1 b).

b) The opening through all discharge pipes and fittings shall have at least the area of the pressure relief device outlet. The characteristics of this downstream system shall be such that the pressure drop (back pressure) will not reduce the relieving capacity below that required or adversely affect the operation of the pressure relief device.

c) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location for disposal of fluids being relieved.

d) Discharge lines from pressure relief devices shall be designed to facilitate drainage and steam venting, or be fitted with drains, to prevent liquid from collecting in the discharge side of a pressure relief device. Drain piping shall discharge to a safe location for the disposal of the fluids being relieved. There are additional requirements specific to boilers and heaters.

e) Where an intervening stop valve is permitted and used, it shall comply with 2.1.1.4.

f) Where a changeover valve is permitted and used, it shall comply with 2.1.1.5.

i) If a muffler is used on a pressure relief valve, it shall have sufficient outlet area to prevent back pressure from interfering with the proper operation and discharge capacity of the valve. The muffler plates or other devices shall be so constructed as to avoid a possibility of restriction of the passages due to deposits. Mufflers shall not be used on high temperature water boiler pressure relief valves.

k) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or

other equipment and, when necessary, lead to a safe location, such as a catchment tank, for the disposal of fluids being relieved.

#### 2.1.1.4 REQUIREMENTS FOR PRESSURE RELIEF STOP VALVES (WHERE PERMITTED)

a4) These stop valves shall be so constructed or positively controlled that the closing of the maximum number of block valves at one time will not reduce the pressure relieving capacity below the required relieving capacity;

<u>2b) Upon specific acceptance of the Jurisdiction, when necessary for the continuous operation of processing</u>

equipment of such a complex nature that shutdown of any part is not feasible, a full area stop valve between a piping system and its pressure relief device may be provided for inspection and repair purposes only. This stop valve shall be arranged so that it can be locked or sealed open and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked or sealed in the open position before the authorized person leaves the station;

<u>3c) A full area stop valve may be placed on the discharge side of a pressure relief device when its</u> discharge is connected to a common header for pressure relief devices to prevent discharges from these other devices from flowing back to the first device during inspection and repair. This stop valve shall be arranged so that it can be locked or sealed open and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked or sealed in the open position before the authorized person leaves the station. This valve shall only be used when a stop valve on the inlet side of the pressure relief device is first closed; or

<u>4d) A piping system where the pressure originates from an outside source may have a stop valve between the system and the pressure relief device, and this valve need not be sealed open, provided it also closes off that vessel from the source of pressure.</u>

# 2.1.1.5 REQUIREMENTS FOR PRESSURE RELIEF CHANGEOVER VALVES (WHERE PERMITTED)

a) A changeover valve, which allows two redundant pressure relief valves to be installed for the purpose of changing from one pressure relief valve to the other while the pressure retaining item is operating, may be used provided the changeover valve is in accordance with the original code of construction. It is recommended that the Jurisdiction be contacted to determine the acceptability of the changeover valves on boiler applications.

b) The changeover valve shall be designed such that there is no intermediate position where both pressure relief valves are isolated from the pressure retaining item.

c) The additional flow restriction caused by a changeover valve shall be considered in the system design.

#### 2.2 PRESSURE RELIEF VALVES FOR POWER BOILERS

See NBIC Part 1, 2.2 for the boilers covered under Part 4, 2.2

#### 2.2.1 GENERAL REQUIREMENTS

a) Only direct spring loaded pressure relief valves or pilot operated pressure relief valves designed to relieve steam shall be used for steam service.

b) Pressure relief valves are valves designed to relieve either steam or water, depending on the application.

c) Pressure relief valves shall be manufactured in accordance with a national or international standard.

dc) Deadweight or weighted-lever pressure relief valves shall not be used.

ed/ For high temperature water boilers, pressure relief valves shall have a closed bonnet, and valve bodies

shall not be constructed of cast iron.

**fe**) Pressure relief valves with an inlet connection greater than NPS 3 (DN 80) and used for pressure greater than 15 psig (100 kPa), shall have a flanged or a welded inlet connection. The dimensions of flanges subjected to boiler pressure shall conform to the applicable standards.

g) When a pressure relief value is exposed to outdoor elements that may affect operation of the value, the value may be shielded with a cover. The cover shall be properly vented and arranged to permit servicing and normal operation of the value.

#### 2.2.2 NUMBER

At least one National Board capacity certified pressure relief valve shall be installed on the boiler<u>in</u> <u>accordance with 2.1.1.1 a)</u>. If the

boiler has more than 500 ft<sub>2</sub> (46 m<sub>2</sub>) of heating surface, or if an electric boiler has a power input of more than

3.76 million BTU/hr (1100 kW), two or more National Board capacity certified pressure relief valves shall be

installed.

#### 2.2.3 LOCATION

a) Pressure relief valves shall be placed on, or as close as physically possible, to the boiler proper. ba) Pressure relief valves shall not be placed on the feedline.

c) Pressure relief valves shall be connected to the boiler independent of any other connection without any unnecessary intervening pipe or fittings. Such intervening pipe or fittings shall not be longer than the face-to-face dimension of the corresponding tee fitting of the same diameter and pressure rating as listed in the applicable standards.

#### 2.2.4 CAPACITY

a) The pressure relief valve capacity for each boiler shall be such that the valve or valves will discharge all

the steam that can be generated by the boiler without allowing the pressure to rise more than 6% above the highest pressure at which any valve is set and in no case to more than 6% above the maximum allowable working pressure of the boiler.

b) The minimum relieving capacity for other than electric boilers and forced-flow steam generators with no fixed steam line and waterline shall be estimated for the boiler and waterwall heating surfaces as given in Table 2.2.4.1, but in no case shall the minimum relieving capacity be less than the maximum designed steaming capacity as determined by the manufacturer.

c) The required relieving capacity in lbs/hr of the pressure relief valves on a high temperature water boiler shall be determined by dividing the maximum output in Btu at the boiler nozzle obtained by the firing of any fuel for which the unit is designed by one thousand.

d) The minimum pressure relief valve relieving capacity for electric boilers shall not be less than 3.5 lbs/hr/

#### kW (1.6 kg/hr/kW) input.

e) If the pressure relief valve capacity cannot be computed, or if it is desirable to prove the computations, it should be checked by any one of the following methods; and if found insufficient, additional relieving capacity shall be provided:

1) By performing an accumulation test, that is, by shutting off all other steam discharge outlets from the boiler and forcing the fires to the maximum. This method should not be used on a boiler with a superheater or reheater or on a high-temperature water boiler.

2) By measuring the maximum amount of fuel that can be burned and computing the corresponding evaporative capacity upon the basis of the heating value of the fuel.

3) By determining the maximum evaporative capacity by measuring the feedwater. The sum of the pressure relief valve capacities marked on the valves shall be equal to or greater than the maximum evaporative capacity of the boiler. This method should not be used on high-temperature water boilers.

#### TABLE 2.2.4.1

MINIMUM POUNDS OF STEAM PER HOUR PER SQUARE FOOT OF HEATING SURFACE LB STEAM/HR FT<sub>2</sub> (KG STEAM/HR M<sub>2</sub>)

#### Firetube Boiler Watertube Boiler

Boiler Heating Surface

Hand-fired 5 (24) 6 (29) Stoker-fired 7 (34) 8 (39) Oil, gas, or pulverized fuel-fired 8 (39) 10 (49) Waterwall Heating Surface Hand-fired 8 (39) 8 (39) Stoker-fired 10 (49) 12 (59) Oil, gas, or pulverized coal 14 (68) 16 (78) Copper-finned Watertubes Hand-fired 4 (20) Stoker-fired 5 (24) Oil, gas, or pulverized fuel-fired 6 (29)

Notes:

When a boiler is fired only by a gas having a heat value not in excess of 200 Btu/ft<sub>3</sub>(7.5MJ/m<sub>3</sub>), the minimum relieving capacity should be based on the values given for hand-fired boilers above.
The heating surface shall be computed for that side of the boiler surface exposed to the products of combustion, exclusive of the superheating surface. In computing the heating surface for this purpose only the tubes, fireboxes, shells, tubesheets, and the projected area of headers need to be considered, except that for vertical firetube steam boilers, only that portion of the tube surface up to the middle gage cock is to be computed.

• For firetube boiler units exceeding 8000 Btu/ft<sub>2</sub> (9085 J/cm<sub>2</sub>) (total fuel Btu (J) Input divided by total heating surface), the factor from the table will be increased by 1 (4.88) for every 1000 Btu/ft.<sub>2</sub> (1136 J/cm<sub>2</sub>) above 8000 Btu/ft.<sub>2</sub> (9085 J/cm<sub>2</sub>) For units less than 7000 Btu/ft<sub>2</sub> (7950 J/cm<sub>2</sub>), the factor from the table will be decreased by 1 (4.88).

• For watertube boiler units exceeding 16000 Btu/ft<sub>2</sub> (18170 J/cm<sub>2</sub>)(total fuel Btu input divided by the total heating surface) the factor from the table will be increased by 1 (4.88) for every 1000 Btu/ft<sub>.2</sub> (1136 J/cm<sub>2</sub>) above 16000 Btu/ft<sub>.2</sub> (18170 J/cm<sub>2</sub>). For units with less than 15000 Btu/ft<sub>.2</sub> (17034 J/cm<sub>2</sub>), the factor in the table will be decreased by 1 (4.88) for every 1000 Btu/ft<sub>.2</sub> (1136 J/cm<sub>2</sub>) below 15000 Btu/ft<sub>.2</sub> (17034 J/cm<sub>2</sub>).

#### 2.2.5 SET PRESSURE

One or more pressure relief valves on the boiler proper shall be set at or below the maximum allowable working pressure. If additional valves are used, the highest pressure setting shall not exceed the maximum

allowable working pressure by more than 3%. The complete range of pressure settings of all the pressure relief valves on a boiler shall not exceed 10% of the highest pressure to which any valve is set. Pressure setting of pressure relief valves on high temperature water boilers may exceed this 10% range.

#### 2.2.6 FORCED-FLOW STEAM GENERATORS

For a forced-flow steam generator with no fixed steamline and waterline, equipped with automatic controls

and protective interlocks responsive to steam pressure, pressure relief valves may be provided in accordance

with the above paragraphs identified in 2.2.5 or the following protection against overpressure shall be provided:

a) One or more power-actuated pressure relief valves shall be provided in direct communication with the boiler when the boiler is under pressure and shall receive a control impulse to open when the maximum allowable working pressure at the superheater outlet is exceeded. The total combined relieving capacity of the power actuated pressure relief valves shall be not less than 10% of the maximum design steaming capacity of the boiler under any operating condition as determined by the manufacturer. The valves shall be located in the pressure part system where they will relieve the overpressure. An isolating stop valve of the outside-screw-and-yoke type should be installed between the power actuated pressure relief valve of the same capacity is so installed as to be in direct communication with the boiler.

b) Pressure relief valves shall be provided having a total combined relieving capacity, including that of the power-actuated pressure relief valve, of not less than 100% of the maximum designed steaming capacity of the boiler, as determined by the manufacturer. In this total, credit in excess of 30% of the

total relieving capacity shall not be allowed for the power-actuated pressure relief valves actually installed. Any or all of the pressure relief valves may be set above the maximum allowable working pressure of the parts to which they are connected, but the set pressures shall be such that when all these valves (together with the power-actuated pressure relief valves) are in operation the pressure will not rise more than 20% above the maximum allowable working pressure of any part of the boiler, except for the steam piping between the boiler and the prime mover.

c) When stop valves are installed in the water steam flow path between any two sections of a forced-flow steam generator with no fixed steamline and waterline:

1) The power-actuated pressure relief valve shall also receive a control impulse to open when the maximum allowable working pressure of the component, having the lowest pressure level upstream to the stop valve, is exceeded.

2) The pressure relief valve shall be located to provide overpressure protection for the component having the lowest working pressure.

3) A reliable pressure-recording device shall always be in service and records kept to provide evidence of conformity to the above requirements.

#### **2.2.7 SUPERHEATERS**

a) Every attached superheater shall have one or more pressure relief valves. The location shall be suitable

for the service intended and shall provide the overpressure protection required. The pressure drop upstream of each pressure relief valve shall be considered in determining the set pressure and relieving capacity of that valve. If the superheater outlet header has a full, free steam passage from end to end and is so constructed that steam is supplied to it at practically equal intervals throughout its length so that there is a uniform flow of steam through the superheater tubes and the header, the pressure relief valve or valves may be located anywhere in the length of header.

b) The pressure-relieving capacity of the pressure relief valve or valves on an attached superheater shall be included in determining the number and size of the pressure relief valves for the boiler provided there are no intervening valves between the superheater pressure relief valve and the boiler and the discharge capacity of the pressure relief valve or valves, on the boiler, as distinct from the superheater, is at least 75% of the aggregate capacity required.

c) Every independently fired superheater that may be shut off from the boiler and permit the superheater to become a fired pressure vessel shall have one or more pressure relief valves having a discharge capacity equal to 6 lbs steam/hr/ft² (29 kg steam/hr/m²) of superheater surface measured on the side exposed to the hot gases.

d) Every pressure relief valve used on a superheater discharging superheated steam at a temperature over 450°F (230°C) shall have a casing, including the base, body, bonnet, and spindle constructed of steel, steel alloy, or equivalent heat-resistant material. The valve shall have a flanged inlet connection or a welding-end inlet connection. The seat and disk shall be constructed of suitable heat-erosive and corrosive-resistant material, and the spring fully exposed outside of the valve casing so that it is protected from contact with the escaping steam.

#### 2.2.8 ECONOMIZERS

An economizer that may not be isolated from a boiler does not require a pressure relief valve. Economizers

that may be isolated from a boiler or other heat transfer device, allowing the economizer to become a fired

pressure vessel, shall have a minimum of one pressure relief valve. Discharge capacity, rated in lbs/hr (kg/

hr), of the pressure relief valve or valves shall be calculated from the maximum expected heat absorption rate in Btu/hr (kJ/hr) of the economizer, and will be determined from manufacturer data, divided by 1,000 Btu/

Ib (2,326 kJ/kg). The pressure relief valve shall be located as close as possible to the economizer outlet. **2.2.9 PRESSURE REDUCING VALVES** 

a) Where pressure reducing valves are used, one or more pressure relief valves shall be installed on the low pressure side of the reducing valve in those installations where the piping or equipment on the low pressure side does not meet the requirements for the steam supply piping.

b) The pressure relief valves shall be located as close as possible to the pressure reducing valve.

c) Capacity of the pressure relief valves shall not be less than the total amount of steam that can pass

from the high pressure side to the low pressure side and be such that the pressure rating of the lower pressure piping or equipment shall not be exceeded.

d) The use of hand-controlled bypasses around reducing valves is permissible. The bypass around a reducing valve may not be greater in capacity than the reducing valve unless the piping or equipment is adequately protected by pressure relief valves or meets the requirements of the high pressure system.
e) See Supplement 1 for additional information on the calculation of the required capacity of pressure relief

valves installed after pressure-reducing valves.

#### 2.2.10 INSTALLATION AND DISCHARGE REQUIREMENTS

a) Every boiler shall have outlet connections for the pressure relief valve, or valves, independent of any other outside steam connection, the area of opening shall be at least equal to the aggregate areas of inlet connections of all of the attached pressure relief valves. An internal collecting pipe, splash plate, or pan should be used, provided the total area for inlet of steam is not less than twice the aggregate areas of the inlet connections of the attached pressure relief valves. The holes in such collecting pipes shall be at least 1/4 in. (6 mm) in diameter, and the least dimension in any other form of opening for inlet of steam shall be 1/4 in. (6 mm). If pressure relief valves are attached to a separate steam drum or dome, the opening between the boiler proper and the steam drum or dome shall be not less than 10 times the total area of the pressure relief valve inlet.

b) Every pressure relief valve shall be connected so as to stand in an upright position with spindle vertical.

c) The opening or connection between the boiler and the pressure relief valve shall have at least the area of the valve inlet and t<u>T</u>he inlet pipe to the pressure relief valve shall <u>be be as short and straight as possible</u>,

no longer than twice the center-to-end (face) dimension of a corresponding tee fitting of the same diameter,

pressure class, and connection type. When a discharge pipe is used, the cross-sectional area shall not be less than the full area of the valve outlet or of the total of the areas of the valve outlets. It shall be as short and straight as possible and arranged to avoid undue stresses on the valve or valves.

d) No valves of any type except a changeover valve in accordance with 2.1.1.5 as defined below shall be placed between the pressure

relief valves and the boiler, nor on the discharge pipe between the pressure relief valves and the atmosphere.

A changeover valve, which allows two redundant pressure relief valves to be installed for the purpose of changing from one pressure relief valve to the other while the boiler is operating, may be used provided the changeover valve is in accordance with the original code of construction. It is recommended that the Jurisdiction be contacted to determine the acceptability of the changeover valves on boiler applications. The changeover valve shall be designed such that there is no intermediate position where both pressure relief valves are isolated from the boiler.

e) When two or more pressure relief valves are used on a boiler, they should be mounted either separately

or as twin valves made by placing individual valves on Y-bases, or duplex valves having two valves in the same body casing. Twin valves made by placing individual valves on Y-bases or duplex valves having two valves in the same body shall be of equal size.

f) When two valves of different sizes are installed singly, the relieving capacity of the smaller valve shall not be less than 50% of that of the larger valve.

g) When a boiler is fitted with two or more pressure relief valves on one connection, this connection to the boiler shall have a cross-sectional area not less than the combined areas of inlet connections of all the pressure relief valves with which it connects.

h) All pressure relief valves shall be piped to a safe point of discharge so located or piped as to be carried clear from running boards or platforms. Provision for an ample gravity drain shall be made in the discharge

pipe at or near each pressure relief valve, and where water or condensation may collect. Each valve shall have an open gravity drain through the casing below the level of the valve seat. For ironand steel- bodied valves exceeding NPS 2 (DN 50), the drain hole shall be tapped not less than NPS 3/8 (DN 10).

i) Discharge piping from pressure relief valves on high temperature water boilers shall have adequate

provisions for water drainage as well as steam venting.

j) If a muffler is used on a pressure relief valve, it shall have sufficient outlet area to prevent back pressure

from interfering with the proper operation and discharge capacity of the valve. The muffler plates or other devices shall be so constructed as to avoid a possibility of restriction of the steam passages due to deposits. Mufflers shall not be used on high temperature water boiler pressure relief valves.

#### 2.2.11 SUPPORTS, FOUNDATIONS, AND SETTINGS

Each boiler pressure relief valve and its associated piping must be safely supported. Design of supports, foundations, and settings shall consider vibration (including seismic where necessary), movement (including

thermal movement), and loadings (including reaction forces) in accordance with jurisdictional requirements,

manufacturer's recommendations, and/or other industry standards, as applicable.

#### 2.3 OVERPRESSURE PROTECTION FOR THERMAL FLUID HEATERS 2.3.1 GENERAL REQUIREMENTS

Thermal fluid heaters shall be provided with overpressure protection in accordance with the code of construction.

#### 2.3.2 PRESSURE RELIEF DEVICES

Thermal fluid heaters shall be equipped with one or more pressure relief devices unless the option for overpressure

protection by system design is utilized (when permitted by the original code of construction). When pressure relief devices are used, the following shall apply:

a) Pressure relief valve(s) shall be of a totally enclosed type and shall not have a lifting lever. A body drain

is not required.

b) Rupture disks may be installed upstream or downstream of the pressure relief valve(s) in accordance with the original code of construction.

c) Pressure relief valves and rupture disks shall be in accordance with the code of construction and designed for liquid, vapor, or combination service as required for the specific installation, service fluids, and overpressure conditions.

cd) The inlet connection to the valve shall be not less than NPS 1/2 (DN 15).

#### 2.3.3 LOCATION

Pressure relief devices shall be connected to the heater in accordance with the original code of construction.

#### 2.3.4 CAPACITY

The pressure relief device(s) shall have sufficient capacity to prevent the pressure vessel from exceeding the

maximum pressure specified in the vessel code of construction.

#### 2.3.5 SET PRESSURE

a) When a single relief device is used, the set pressure marked on the device shall not exceed the maximum

allowable working pressure.

b) When more than one pressure relief device is provided to obtain the required capacity, only one pressure

relief device set pressure needs to be set at or below the maximum allowable working pressure. The set pressure of the additional relief devices shall be such that the pressure cannot exceed the maximum

pressure permitted by the code of construction.

#### 2.3.6 INSTALLATION

a) When a discharge pipe is used, the cross sectional area shall not be less than the full area of the valve outlet. The size of the discharge lines shall be such that any pressure that may exist or develop will not reduce the relieving capacity or adversely affect the operation of the attached pressure vessel relief devices. Discharge piping shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief device.

b) The cross sectional area of the piping between the heater and the relief device shall be sized either to

avoid restricting the flow to the pressure relief devices or made at least equal to the inlet area of the pressure relief devices connected to it.

c) When two or more required pressure relief devices are placed on one connection, the inlet crosssectional

area of this connection shall be sized either to avoid restricting the flow to the pressure relief devices or made at least equal to the combined inlet areas of the pressure relief devices connected to it.

d) Unless permitted by the code of construction, there shall be no intervening stop valve between the vessel and its pressure relief device(s), or between the pressure relief device and the point of discharge.

e) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location, such as a catchment tank, for the disposal of fluids being relieved.

f) Discharge lines from pressure relief devices shall be designed to facilitate drainage or be fitted with low point or valve body drains to prevent liquid from collecting in the discharge side of a pressure relief device. Drain piping shall discharge to a safe location for the disposal of the fluids being relieved.

g) The pressure relief discharge should be connected to a closed, vented storage tank or blowdown tank with solid piping (no drip pan elbow, or other air gap). When outdoor discharge is used, the following should be considered for discharge piping at the point of discharge:

1) Both thermal and chemical reactions (personnel hazard);

2) Combustible materials (fire hazard);

3) Surface drains (pollution and fire hazard);

4) Loop seal or rain cap on the discharge (keep both air and water out of the system);

5) Drip leg near device (prevent liquid collection); and

6) Heat tracing for systems using high freeze point fluids (prevent blockage).

h) A suitable condenser that will condense all the vapors discharged from the pressure relief valve may be

used in lieu of piping the vapors to the atmosphere.

i) In order to minimize the loss by leakage of material through the pressure relief valve, a rupture disk may be installed between the pressure relief valve and the vaporizer, provided the following requirements are met:

1) The cross-sectional area of the connection to a vaporizer shall be not less than the required relief area of the rupture disk.

2) The maximum pressure of the range for which the disk is designed to rupture shall not exceed the opening pressure for which the pressure relief valve is set or the maximum allowable working pressure of the vessel.

3) The opening provided through the rupture disk, after breakage, shall be sufficient to permit a flow equal to the capacity of the attached valve, and there is no chance of interference with the proper functioning of the valve, but in no case shall this area be less than the inlet area of the valve.

4) The space between a rupture disk and the valve shall be provided with a pressure gage, try cock, free vent, or a suitable telltale indicator. This arrangement permits the detection of disk rupture or leakage.

j) Pressure relief valve discharge capacity shall be determined from the following equation:

 $W = CKAP \sqrt{(M/T)}$ 

Where:

A = discharge area of pressure relief valve

C = constant for vapor that is a function of the ratio of specific heats  $k = c_p/c_v$ .

**Note:** Where k is not known, k = 1.001.

K = coefficient of discharge for the valve design

M = molecular weight

P = (set pressure × 1.03) + Atmosphere Pressure

T = absolute temperature at inlet, °F + 460 (°C + 273)

W = flow of vapor

The required minimum pressure relief valve relieving capacity shall be determined from the following equation:

 $W = C \times H \times 0.75/h$ 

Where:

C = maximum total weight or volume of fuel burned per hour,  $lb (kg) or ft_3 (m_3)$ 

H = heat of combustion of fuel, Btu/lb (J/kg) or Btu/ft<sub>3</sub> (J/m<sub>3</sub>)

h = latent heat of heat transfer fluid at relieving pressure, Btu/lb (J/kg)

W = weight of organic fluid vapor generated per hour

# The sum of the pressure relief valve capacities marked on the valves shall be equal to or greater than W. **2.4 PRESSURE RELIEF VALVES FOR STEAM HEATING, HOT WATER HEATING, AND HOT WATER SUPPLY BOILERS**

See NBIC Part 1, 3.2 for the scope of pressure retaining items covered by Part 4, 2.4.

#### 2.4.1 GENERAL REQUIREMENTS

The following general requirements pertain to the installation of pressure relief valves on heating boilers.

#### 2.4.1.1 INSTALLATION OF PRESSURE RELIEF VALVES FOR HEATING BOILERS 2.4.1.1.1 PERMISSIBLE INSTALLATION

Pressure relief valves shall be located at the top side of the boiler. The top side of the boiler shall mean the

highest practicable part of the boiler proper but in no case shall the pressure relief valves be located below the

normal operating level and in no case shall the pressure relief valve be located below the lowest permissible

water level. They shall be connected directly to a tapped or flanged opening in the boiler, to a fitting connected

to the boiler by a short nipple, to a Y-base, or to a valveless header connecting steam or water outlets on the

same boiler. Coil or header type boilers shall have the pressure relief valve located on the steam or hot water

outlet end. Pressure relief valves shall be installed with their spindles vertical. The opening or connection between the boiler and any pressure relief valve shall have at least the area of the valve inlet.

# 2.4.1.1.2 REQUIREMENTS FOR COMMON CONNECTIONS FOR TWO OR MORE VALVES

a) When a boiler is fitted with two or more pressure relief valves on one connection, this connection shall have a cross-sectional area not less than the combined areas of inlet connections of all the pressure relief valves with which it connects.

**ba**) When a Y-base is used, the inlet area shall be not less than the combined outlet areas. When the size of the boiler requires a pressure relief valve larger than NPS 4 (DN 100), two or more valves having the required combined capacity shall be used. When two or more valves are used on a boiler, they may be single, directly attached, or installed on a Y-base.

#### 2.4.1.2 THREADED CONNECTIONS

A threaded connection may be used for attaching a valve.

#### 2.4.1.3 PROHIBITED INSTALLATIONS

Pressure relief valves shall not be connected to an internal pipe in the boiler.

#### 2.4.1.4 USE OF SHUTOFF VALVES PROHIBITED

No shutoff valve of any description shall be placed between the pressure relief valve and the boiler or on discharge pipes between such valves and the atmosphere.

#### 2.4.1.5 PRESSURE RELIEF VALVE DISCHARGE PIPING

a) A discharge pipe shall be used. Its internal cross-sectional area shall be not less than the full area of the valve outlet or of the total of the valve outlets that discharge into the pipe, and shall be as short and straight as possible and arranged as to avoid undue stress on the valve or valves. A union may be installed in the discharge piping close to the valve outlet. When an elbow is placed on a pressure relief valve discharge pipe, it shall be located close to the valve outlet downstream of the union to minimize reaction moment stress.

b) The discharge from pressure relief valves shall be so arranged that there will be no danger of scalding attendants. The pressure relief valve discharge shall be piped away from the boiler to a safe point of discharge, and there shall be provisions made for properly draining the piping. The size and arrangement of discharge piping shall be such that any pressure that may exist or develop will not reduce the relieving capacity of the relieving devices below that required to protect the boiler.

#### 2.4.1.6 TEMPERATURE AND PRESSURE RELIEF VALVES

Hot-water heating or supply boilers limited to a water temperature of 210°F (99°C) may have one or more National Board capacity certified temperature and pressure relief valve(s) installed. The requirements of 2.4.1.1 through 2.4.1.5 shall be met, except as follows:

a) A Y-type fitting shall not be used.

b) If additional valves are used, they shall be temperature and pressure relief valves.

c) When the temperature and pressure relief valve is installed directly on the boiler with no more than 4 in.

(100 mm) maximum interconnecting piping, the valve may be installed in the horizontal position with the outlet pointed down.

#### 2.4.2 PRESSURE RELIEF VALVE REQUIREMENTS FOR STEAM HEATING BOILERS

a) Pressure relief valves shall be manufactured in accordance with a national or international standard. b) Each steam boiler shall have one or more National Board capacity certified pressure relief valves of the spring pop type adjusted and sealed to discharge at a pressure not to exceed 15 psig (100 kPa).

c) No pressure relief valve for a steam boiler shall be smaller than NPS 1/2 (DN 15). No pressure relief valve shall be larger than NPS 4 (DN 100). The inlet opening shall have an inside diameter equal to, or greater than, the seat diameter.

d) The minimum valve capacity in lbs/hr (kg/hr) shall be the greater of that determined by dividing the maximum Btu/hr (W) output at the boiler nozzle obtained by the firing of any fuel for which the unit is installed by 1,000 Btu/hr/lb (645 W/kg), or shall be determined on the basis of the lbs steam/hr/ft<sub>2</sub> (kg steam/hr/m<sub>2</sub>) of boiler heating surface as given in Table 2.2.4.1. For cast-iron boilers, the minimum valve capacity shall be determined by the maximum output method. In many cases a greater relieving capacity of valves will have to be provided than the minimum specified by these rules. In every case, the requirement of 2.4.2 e) shall be met.

e) The pressure relief valve capacity for each steam boiler shall be such that with the fuel burning equipment

installed, and operated at maximum capacity, the pressure cannot rise more than 5 psig (34 kPa) above the maximum allowable working pressure.

f) When operating conditions are changed, or additional boiler heating surface is installed, the valve capacity shall be increased, if necessary, to meet the new conditions and be in accordance with 2.4.2 e). The additional valves required, on account of changed conditions, may be installed on the outlet piping provided there is no intervening valve.

#### 2.4.3 PRESSURE RELIEF VALVE REQUIREMENTS FOR HOT WATER HEATING OR HOT WATER SUPPLY BOILERS

a) Pressure relief valves shall be manufactured in accordance with a national or international standard.
b) Each hot-water heating or hot-water supply boiler shall have at least one National Board capacity certified pressure relief valve, of the automatic reseating type set to relieve at or below the maximum allowable working pressure of the boiler.

c) Hot-water heating or hot-water supply boilers limited to a water temperature not in excess of 210°F (99°C) may have, in lieu of the valve(s) specified in (b) above, one or more National Board capacity certified

temperature and pressure relief valves of the automatic reseating type set to relieve at or below the maximum allowable working pressure of the boiler.

d) When more than one pressure relief valve is used on either hot-water heating or hot water supply boilers,

the additional valves shall be National Board capacity certified and may have a set pressure within a range not to exceed 6 psig (40 kPa) above the maximum allowable working pressure of the boiler up to and including 60 psig (414 kPa), and 5% for those having a maximum allowable working pressure exceeding 60 psig (414 kPa).

e) No pressure relief valve shall be smaller than NPS 3/4 (DN 20) nor larger than NPS 4 (DN 100), except that boilers having a heat input not greater than 15,000 Btu/hr (4.4 kW) should be equipped with a rated pressure relief valve of NPS 1/2 (DN 15).

f) The required relieving capacity, in lbs/hr (kg/hr), of the pressure relief valve(s) on a boiler shall be the greater of that determined by dividing the maximum output in Btu/hr (W) at the boiler nozzle obtained by the firing of any fuel for which the unit is installed by 1,000 Btu//hr/lb (645 W/kg), or shall be determined

on the basis of lbs steam/hr/ft<sub>2</sub> (kg steam/hr/m<sub>2</sub>) as given in Table 2.2.4.1. For cast-iron boilers, the minimum valve capacity shall be determined by the maximum output method. In many cases a greater relieving capacity of valves will have to be provided than the minimum specified by these rules. In every case, the requirements of 2.4.3 h) shall be met.

g) When operating conditions are changed, or additional boiler heating surface is installed, the valve capacity shall be increased, if necessary, to meet the new conditions and be in accordance with 2.4.3 h). The additional valves required, on account of changed conditions, may be installed on the outlet piping provided there is no intervening valve.

h) Pressure relief valve capacity for each boiler with a single pressure relief valve shall be such that, with the fuel burning equipment installed and operated at maximum capacity, the pressure cannot rise more than 10% above the maximum allowable working pressure. When more than one pressure relief valve is used, the over pressure shall be limited to 10% above the set pressure of the highest set valve allowed by 2.4.3 b).

# 2.4.4 TEMPERATURE AND PRESSURE RELIEF VALVE REQUIREMENTS FOR POTABLE WATER HEATERS

a) Each water heater shall have at least one National Board capacity certified temperature and pressure relief valve. No temperature and pressure relief valve shall be smaller than NPS 3/4 (DN 20).

b) The pressure setting shall be less than or equal to the maximum allowable working pressure of the water heater. However, if any of the other components in the hot-water supply system (such as valves, pumps, expansion or storage tanks, or piping) have a lesser working pressure rating than the water heater, the pressure setting for the temperature and pressure relief valve(s) shall be based upon the component with the lowest maximum allowable working pressure rating. If more than one temperature and relief valve is used, the additional valve(s) may be set within a range not to exceed 10% above the set pressure of the first valve.

c) The required relieving capacity in Btu/hr (W) of the temperature and pressure relief valve shall not be less than the maximum allowable input unless the water heater is marked with the rated burner input capacity of the water heater on the casing in a readily visible location, in which case the rated burner input capacity may be used as a basis for sizing the temperature and pressure relief valves. The relieving capacity for electric water heaters shall be 3500 Btu/hr (1.0 kW) per kW of input. In every case, the following requirements shall be met. Temperature and pressure relief valve capacity for each water heater shall be such that with the fuel burning equipment installed and operating at maximum capacity, the pressure cannot rise more than 10% above the maximum allowable working pressure.

Many temperature and pressure relief valves have a National Board capacity certified rating which was determined according to ASME Code requirements, and a lower Canadian Standards Association (CSA) rating value. Where the ASME Code is the only referenced code of construction the National Board capacity certified rating may be used. If the water heater is not an ASME vessel, or the CSA rating is required by another standard (such as a plumbing or building code) then that rating shall be used. d) If operating conditions are changed or additional heating surface is installed, the temperature and pressure

relief valve capacity shall be increased, if necessary, to meet the new conditions and shall be in accordance with the above provisions. In no case shall the increased input capacity exceed the maximum allowable input capacity. The additional valves required, on account of changed conditions, may be installed on the outlet piping providing there is no intervening valve.

#### 2.4.4.1 INSTALLATION

Temperature and pressure relief valves shall be installed by either the installer or the manufacturer before a

water heater is placed in operation.

#### 2.4.4.2 PERMISSIBLE INSTALLATIONS

Temperature and pressure relief valves shall be connected directly to a tapped or flanged opening in the top

of the water heater, to a fitting connected to the water heater by a short nipple, to a Y-base, or to a valveless

header connecting water outlets on the same heater. Temperature and pressure relief valves shall be installed

with their spindles upright and vertical with no horizontal connecting pipe, except that, when the temperature

and pressure relief valve is installed directly on the water heater vessel with no more than 4 in. (100 mm) maximum interconnecting piping, the valve may be installed in the horizontal position with the outlet pointed

down. The center line of the temperature and pressure relief valve connection shall be no lower than 4 in. (100 mm) from the top of the shell. No piping or fitting used to install the temperature and pressure relief valve

shall be of nominal pipe size less than that of the valve inlet.

#### 2.4.4.3 REQUIREMENTS FOR COMMON CONNECTION FOR TWO OR MORE VALVES

a) When a potable water heater is fitted with two or more temperature and pressure relief valves on one connection, this connection shall have a cross sectional area not less than the combined areas of inlet connections of all the temperature and pressure relief valves with which it connects.

b) When a Y-base is used, the inlet area shall be not less than the combined outlet areas.

c) When the size of the water heater requires a temperature and pressure relief valve larger than NPS 4 (DN 100) two or more valves having the required combined capacity shall be used. When two or more valves are used on a water heater, they may be single, directly attached, or installed on a Y-base.

#### 2.4.4.4 THREADED CONNECTIONS

A threaded connection may be used for attaching a temperature and pressure relief valve.

#### 2.4.4.5 PROHIBITED INSTALLATIONS

Temperature and pressure relief valves shall not be connected to an internal pipe in the water heater or a cold

water feed line connected to the water heater.

#### 2.4.4.6 USE OF SHUTOFF VALVES PROHIBITED

No shutoff valve of any description shall be placed between the temperature and pressure relief valve and the

water heater or on discharge pipes between such valves and the atmosphere.

#### 2.4.4.7 TEMPERATURE AND PRESSURE RELIEF VALVE DISCHARGE PIPING

a) The discharge from temperature and pressure relief valves shall be so arranged that there will be no danger of scalding attendants. When the temperature and pressure relief valve discharge is piped away from the water heater to the point of discharge, there shall be provisions for properly draining the piping and valve body. The size and arrangement of discharge piping shall be such that any pressure that may exist or develop will not reduce the relieving capacity of the relieving devices below that required to protect

the water heater.

b) When a discharge pipe is used, it shall be not less than the nominal size of the valve outlet and shall be as short and straight as possible and so arranged as to avoid undue stress on the valve. When an elbow is placed on a temperature and pressure relief discharge pipe, it shall be located close to the valve outlet.

c) Where multiple valves relieve into a common discharge pipe, the cross-sectional flow area of the common discharge pipe shall be equal to or greater than the sum of the individual temperature and pressure valve discharge pipe areas.

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# 2.4.5 PRESSURE RELIEF VALVES FOR TANKS AND HEAT EXCHANGERS 2.4.5.1 STEAM TO HOT-WATER SUPPLY

When a hot-water supply is heated indirectly by steam in a coil or pipe within the service limitations set forth

in Part 1, 3.2, *Definitions*, the pressure of the steam used shall not exceed the safe working pressure of the

hot water tank, and a pressure relief valve at least NPS 1 (DN 25), set to relieve at or below the maximum allowable working pressure of the tank, shall be applied on the tank.

#### 2.4.5.2 HIGH TEMPERATURE WATER TO WATER HEAT EXCHANGER

When high temperature water is circulated through the coils or tubes of a heat exchanger to warm water for

space heating or hot-water supply, within the service limitations set forth in Part 1, 3.2, *Definitions*, the heat

exchanger shall be equipped with one or more National Board capacity certified pressure relief valves set to

relieve at or below the maximum allowable working pressure of the heat exchanger, and of sufficient rated

capacity to prevent the heat exchanger pressure from rising more than 10% above the maximum allowable

working pressure of the vessel.

#### 2.4.5.3 HIGH TEMPERATURE WATER TO STEAM HEAT EXCHANGER

When high temperature water is circulated through the coils or tubes of a heat exchanger to generate low pressure steam, within the service limitations set forth in Part 1, 3.2, *Definitions*, the heat exchanger shall be

equipped with one or more National Board capacity certified pressure relief valves set to relieve at a pressure

not to exceed 15 psig (100 kPa), and of sufficient rated capacity to prevent the heat exchanger pressure from rising more than 5 psig (34 kPa) above the maximum allowable working pressure of the vessel. For heat exchangers requiring steam pressures greater than 15 psig (100 kPa), refer to NBIC Part 1, Section 2

or Section 4.

#### 2.5 PRESSURE VESSEL PRESSURE RELIEF DEVICES

See NBIC Part 1, 4.1 for the scope of pressure vessels covered by the requirements of Part 4, 2.5. Pressure relief devices protecting pressure vessels shall meet the following requirements:

#### 2.5.1 DEVICE REQUIREMENTS

a) Pressure relief devices shall be manufactured in accordance with a national or international standard and be certified for capacity or flow resistance by the National Board.

b) Dead weight or weighted lever pressure relief valves shall not be used.

c) An unfired steam boiler shall be equipped with pressure relief valves as required in NBIC Part 4, 2.2.

d) Pressure relief devices shall be selected (i.e., material, pressure, etc.) and installed such that their proper functioning will not be hindered by the nature of the vessel's contents.

#### 2.5.2 NUMBER OF DEVICES

At least one device shall be provided for protection of a pressure vessel. Pressure vessels with multiple chambers

with different maximum allowable working pressures shall have a pressure relief device to protect each chamber under the most severe coincident conditions.

#### 2.5.3 LOCATION

a) The pressure relief device shall be installed directly on the pressure vessel, unless the source of pressure

is external to the vessel and is under such positive control that the pressure cannot exceed the maximum overpressure permitted by the original code of construction and the pressure relief device cannot be isolated from the vessel, except as permitted by 2.5.6 e) 2).

b) Pressure relief devices intended for use in compressible fluid service shall be connected to the vessel in the vapor space above any contained liquid or in the piping system connected to the vapor space. c) Pressure relief devices intended for use in liquid service shall be connected below the normal liquid line.

The liquid level during upset conditions shall be considered.

#### 2.5.4 CAPACITY

a) The pressure relief device(s) shall have sufficient capacity to ensure that the pressure vessel is not exposed to pressure greater than that specified in the original code of construction.

b) Pressure vessels that can be exposed to fire or other sources of unexpected external heat may require supplemental pressure relief devices to provide additional relieving capacity.

1) The combined capacity of all installed pressure relief devices shall be adequate to prevent the pressure

from rising more than 21% above maximum allowable working pressure.

2) The set point of any supplemental pressure relief device(s) shall not exceed 110% of the maximum allowable working pressure. If a single pressure relief device is utilized to protect the vessel during both operational and fire or other unexpected external heating conditions, the set point shall not exceed maximum allowable working pressure.

c) Vessels connected together by a system of piping not containing valves that can isolate any pressure vessel may be considered as one unit when determining capacity requirements.

d) Heat exchangers and similar vessels shall be protected with a pressure relief device of sufficient capacity

to avoid overpressure in case of internal failure.

#### 2.5.5 SET PRESSURE

a) When a single pressure relief device is used, the set pressure marked on the device shall not exceed the maximum allowable working pressure.

b) When more than one pressure relief device is provided to obtain the required capacity, only one pressure relief device set pressure needs to be at the maximum allowable working pressure. The set pressures of the additional pressure relief devices shall be such that the pressure cannot exceed the overpressure permitted by the code of construction.

#### 2.5.6 INSTALLATION AND DISCHARGE PIPING REQUIREMENTS

a) The opening through all pipe and fittings between a pressure vessel and its pressure relief device shall have at least the area of the pressure relief device inlet. The characteristics of this upstream system shall be such that the pressure drop will not reduce the relieving capacity below that required or adversely affect the proper operation of the pressure relief device. When a discharge pipe is used, the size shall be such that any pressure that may exist or develop will not reduce the relieving capacity below that any pressure that may exist or develop will not reduce the relieving capacity below that required or adversely affect the proper operation of the pressure relief device. It shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief device. b) A non-reclosing device installed between a pressure vessel and a pressure relief valve shall meet the requirements of 2.5.6 a).

c) The opening in the pressure vessel wall shall be designed to provide unobstructed flow between the vessel and its pressure relief device.

d) When two or more required pressure relief devices are placed on one connection, the inlet crosssectional

area of this connection shall be sized either to avoid restricting flow to the pressure relief devices or made at least equal to the combined inlet areas of the pressure relief devices connected to it. The flow characteristics of the upstream system shall satisfy the requirements of 2.5.6 a).

e) There shall be no intervening stop valves between the vessel and its pressure relief device(s), or between the pressure relief device(s) and the point of discharge, except under the following conditions:
1) When these stop valves are so constructed or positively controlled that the closing of the maximum number of block valves at one time will not reduce the pressure relieving capacity below the required relieving capacity.

2) Upon specific acceptance of the Jurisdiction, when necessary for the continuous operation of processing

equipment of such a complex nature that shutdown of any part is not feasible, a full area stop valve between a pressure vessel and its pressure relief device may be provided for inspection and repair purposes only. This stop valve shall be arranged so that it can be locked or sealed open, and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked or sealed in the open position before the authorized person leaves the station.

3) A full area stop valve may also be placed on the discharge side of a pressure relief device when its discharge is connected to a common header for pressure relief devices to prevent discharges from these other devices from flowing back to the first device during inspection and repair. This stop valve shall be arranged so that it can be locked or sealed open, and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked and sealed in the open position before the authorized person leaves the station. This valve shall only be used when a stop valve on the inlet side of the pressure relief device is first closed.

4) A pressure vessel in a system where the pressure originates from an outside source may have a stop valve between the vessel and the pressure relief device, and this valve need not be sealed

open, provided it also closes off that vessel from the source of the pressure.

5) Pressure vessels designed for human occupancy (such as decompression or hyperbaric chambers) shall be provided with a quick opening stop valve between the pressure vessel and its pressure relief valve. The stop valve shall be normally sealed open with a frangible seal and be readily accessible to the pressure relief attendant.

f) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location for disposal of fluids being relieved.

g) Discharge lines from pressure relief devices shall be designed to facilitate drainage or be fitted with drains to prevent liquid from collecting in the discharge side of a pressure relief device. The size of discharge lines shall be such that any pressure that may exist or develop will not reduce the relieving capacity of the pressure relief device or adversely affect the operation of the pressure relief device. It shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief device.

h) Pressure relief devices shall be installed so they are readily accessible for inspection, repair, or replacement.

i) Pressure vessel pressure relief devices and discharge piping shall be safely supported. The reaction forces due to discharge of pressure relief devices shall be considered in the design of the inlet and discharge

piping. Design of supports, foundations, and settings shall consider vibration (including seismic where necessary), movement (including thermal movement), and loadings (including reaction forces during device operation in accordance with jurisdictional requirements, manufacturer's recommendations, and/or other industry standards, as applicable.

# 2.5.7 TEMPERATURE AND PRESSURE RELIEF DEVICES FOR HOT WATER STORAGE TANKS

a) Each hot water storage tank shall be equipped with an ASME/NB certified temperature and pressure relief device set at a pressure not to exceed the maximum allowable working pressure and 210°F. (99°C).

b) The temperature and pressure relief device shall meet the requirements of 2.5.1 through 2.5.6 above. **2.6 PIPING SYSTEM PRESSURE RELIEF DEVICES** 

See NBIC Part 1, Section 5 for the piping systems associated with Part 4, 2.6.

When required by the original code of construction, piping shall be protected by pressure relief devices in accordance with the following requirements.

#### 2.6.1 DEVICE REQUIREMENTS

a) Pressure relief devices shall be manufactured in accordance with a national or international standard and be certified for capacity or flow resistance by the National Board.

1) In certain cases piping codes of construction permit the use of regulators, which may include integral pressure relief valves to limit the pressure in a piping system. In this case, capacity certification of the pressure relief valve is not required.

2) Some piping codes of construction permit the use of pressure relief devices without capacity certification.

In this case, capacity certification of the pressure relief device by the National Board is not required.

b) Dead weight or weighted lever pressure relief devices shall not be used.

c) Pressure relief devices shall be selected (i.e., material, pressure, etc.) and installed such that their proper functioning will not be hindered by the nature of the piping system's contents.

#### 2.6.2 NUMBER OF DEVICES

At least one pressure relief device shall be provided for protection of a piping system. A pressure relief device

installed on a pressure vessel or other component connected to the piping system may be used to meet this

requirement. Portions of piping systems with different maximum allowable working pressures shall have a pressure relief device to protect each portion separately.

#### 2.6.3 LOCATION

Pressure relief devices, except those covered by NBIC Part 4, 2.1 through 2.2, may be installed at any

location in the system provided the pressure in any portion of the system cannot exceed the maximum overpressure

permitted by the original code of construction. Pressure drop to the pressure relief device under flowing conditions shall be considered when determining pressure relief device location. The pressure relief

device shall not be isolated from the piping system except as permitted by 2.6.6 e).

#### 2.6.4 CAPACITY

a) The pressure relief device(s) shall have sufficient capacity to ensure that the piping is not exposed to pressures greater than that specified in the original code of construction.

b) When a non-reclosing device is installed between a pressure relief valve and the pipe, the reduction in capacity due to installation of the non-reclosing device shall be determined in accordance with the code of construction by use of a National Board certified Combination Capacity Factor (CCF). For rupture disks, if a certified combination capacity factor is not available, the capacity of the pressure relief valve shall be multiplied by 0.9 and this value used as the capacity of the combination installation. c) The owner shall document the basis for selection of the pressure relief devices used, including capacity,

and have such calculations available for review by the Jurisdiction, when required.

#### 2.6.5 SET PRESSURE

a) When a single pressure relief device is used, the set pressure marked on the device shall not exceed the maximum allowable working pressure, except when allowed by the original code of construction.b) When more than one pressure relief device is provided to obtain the required capacity, only one pressure

relief device set pressure need be at or below the maximum allowable working pressure. The set pressures of the additional pressure relief devices shall be such that the pressure cannot exceed the overpressure permitted by the code of construction.

#### 2.6.6 INLET AND DISCHARGE PIPING REQUIREMENTS

a) The opening through all pipes and fittings between a piping system and its pressure relief device shall have at least the area of the pressure relief device inlet. The characteristics of this upstream system shall be such that the pressure drop will not reduce the relieving capacity below that required or adversely affect the operation of the pressure relief device.

b) A non-reclosing device installed between a piping system and a pressure relief valve shall meet the requirements of 2.6.6 a).

c) The opening in the pipe shall be designed to provide unobstructed flow between the pipe and its pressure

relief device.

d) When two or more required pressure relief devices are placed on the connection, the inlet crosssectional

area of this connection shall be sized either to avoid restricting flow to the pressure relief devices or made at least equal to the combined inlet areas of the pressure relief devices connected to it. The flow characteristics of the upstream system shall satisfy the requirements of 2.6.6 a).

e) There shall be no intervening stop valves between the piping system and its pressure relief device(s), or

between the pressure relief device(s) and the point of discharge except under the following conditions:

1) These stop valves shall be so constructed or positively controlled that the closing of the maximum number of block valves at one time will not reduce the pressure relieving capacity below the required relieving capacity;

2) Upon specific acceptance of the Jurisdiction, when necessary for the continuous operation of processing

equipment of such a complex nature that shutdown of any part is not feasible, a full area stop valve between a piping system and its pressure relief device may be provided for inspection and repair purposes only. This stop valve shall be arranged so that it can be locked or sealed open and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked or sealed in the open position before the authorized person leaves the station;

3) A full area stop valve may be placed on the discharge side of a pressure relief device when its

discharge is connected to a common header for pressure relief devices to prevent discharges from these other devices from flowing back to the first device during inspection and repair. This stop valve shall be arranged so that it can be locked or sealed open and it shall not be closed except by an authorized person who shall remain stationed there during that period of operation while the valve remains closed. The valve shall be locked or sealed in the open position before the authorized person leaves the station. This valve shall only be used when a stop valve on the inlet side of the pressure relief device is first closed; or

4) A piping system where the pressure originates from an outside source may have a stop valve between the system and the pressure relief device, and this valve need not be sealed open, provided it also closes off that vessel from the source of pressure.

f) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location for disposal of fluids being relieved. g) Discharge lines from pressure relief devices shall be designed to facilitate drainage or be fitted with drains to prevent liquid from collecting in the discharge side of a pressure relief device. The size of discharge lines shall be such that any pressure that may exist or develop will not reduce the relieving capacity of the pressure relief device or adversely affect the operation of the pressure relief device. It shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief device.

h) The reaction forces due to discharge of pressure relief devices shall be considered in the design of the inlet and discharge piping.

i) Pressure relief devices shall be installed so they are accessible for inspection, repair, or replacement.

#### Part 4:

#### 2.4.4.3 REQUIREMENTS FOR COMMON CONNECTION FOR TWO OR MORE VALVES

- a) When a potable water heater is fitted with two or more temperature and pressure relief valves on one connection, this connection shall have a cross sectional area not less than the combined areas of inlet connections of all the temperature and pressure relief valves with which it connects.
- b) When a Y-base is used, the inlet area shall be not less than the combined outlet areas.
- c)b) When the size of the water heater requires a temperature and pressure relief valve larger than NPS 4 (DN 100) two or more valves having the required combined capacity shall be used. When two or more valves are used on a water heater, they may be single, directly attached, or installed on a Y-base.

#### Part 1:

#### 3.9.4.3 REQUIREMENTS FOR COMMON CONNECTION FOR TWO OR MORE VALVES

- a) When a potable water heater is fitted with two or more temperature and pressure relief valves on one connection, this connection shall have a cross sectional area not less than the combined areas of inlet connections of all the temperature and pressure relief valves with which it connects.
- b) When a Y-base is used, the inlet area shall be not less than the combined outlet areas.
- c)b) When the size of the water heater requires a temperature and pressure relief valve larger than NPS 4 (DN 100) two or more valves having the required combined capacity shall be used. When two or more valves are used on a water heater, they may be single, directly attached, or installed on a Y-base.

#### ITEM 18-73 Proposal Rev. 3/25/20

#### PART 4

#### 2.3 OVERPRESSURE PROTECTION FOR THERMAL FLUID HEATERS

#### 2.3.1 GENERAL REQUIREMENTS

Thermal fluid heaters shall be provided with overpressure protection in accordance with the code of construction.

#### 2.3.2 PRESSURE RELIEF DEVICESVALVES

Thermal fluid heaters shall be equipped with one or more pressure relief <u>devices valves</u> unless the option for overpressure protection by system design is utilized (when permitted by the original code of construction). When pressure relief <u>devices valves</u> are used, the following shall apply:

a) Pressure relief valve(s) shall be of a totally enclosed type, and shall not have a lifting lever. A body drain is not required.

b) A lifting lever shall not be used in pressure relief valve(s). A body drain is not required.

b) Rupture disks may be installed upstream or downstream of the pressure relief valve(s) in accordance with the original code of construction.

c) Pressure relief valves and rupture disks shall be in accordance with the code of construction and designed for liquid, vapor, or combination service as required for the specific installation, service fluids, and overpressure conditions.

d) Cast iron fittings shall not be used.

e) Copper and copper alloys shall not be used.

df) The inlet connection to the valve shall be not less than NPS ½ (DN 15).

#### 2.3.3 LOCATION

Pressure relief <u>devices valves</u> shall be connected to the heater in accordance with the original code of construction.

#### 2.3.4 CAPACITY

The pressure relief <u>device(s)valve(s)</u> shall have sufficient capacity to prevent the pressure vessel from exceeding the maximum pressure specified in the vessel code of construction.

#### 2.3.5 SET PRESSURE

a) When a single relief <u>device valve</u> is used, the set pressure marked on the device shall not exceed the maximum allowable working pressure.

b) When more than one pressure relief <u>device-valve</u> is provided to obtain the required capacity, only one pressure relief <u>device-valve</u> set pressure needs to be set at or below the maximum allowable working

pressure. The set pressure of the additional relief <u>devices valves</u> shall be such that the pressure cannot exceed the maximum pressure permitted by the code of construction.

#### 2.3.6 INSTALLATION

Pressure relief valves and the associated discharge piping shall be installed in accordance with the heater Manufacturer's recommendations. The installation of the pressure relief valves required for Thermal Fluid Heaters shall include but not be limited to following requirements:

a) <u>The pressure relief valve shall be provided with discharge piping.</u> When a discharge pipe is used, t<u>T</u>he cross-sectional area <u>of discharge piping</u> shall not be less than the full area of the valve outlet. The size of the discharge lines shall be such that any pressure that may exist or develop will not reduce the relieving capacity or adversely affect the operation of the attached pressure vessel relief <u>devicesvalves</u>. Discharge piping shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief <u>devicevalve</u>.

b) The pressure relief valve shall be connected to the pressure vessel in accordance with the original code of construction.

**b**<u>c</u>) The cross sectional area of the piping between the heater and the relief device shall be sized either to avoid restricting the flow to the pressure relief devices or made at least equal to the inlet area of the pressure relief devices connected to it.

ed) When two or more required pressure relief devices are placed on one connection, the inlet crosssectional area of this connection shall be sized either to avoid restricting the flow to the pressure relief devices or made at least equal to the combined inlet areas of the pressure relief devices connected to it.

<u>de</u>) Unless permitted by the code of construction, there shall be no intervening stop valve between the vessel and its pressure relief device(s), or between the pressure relief device and the point of discharge.

ef) Pressure relief device discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location, such as a catchment tank, for the disposal of fluids being relieved.

fg) Discharge lines from pressure relief devices valves shall be designed to facilitate drainage or be fitted with low point or valve body drains to prevent liquid from collecting in the discharge side of a pressure relief device. Drain piping shall discharge to a safe location for the disposal of the fluids being relieved. The possibility of solidification of fluid leakage into the discharge piping system shall be considered.

<u>gh</u>) The pressure relief discharge should shall be connected to a closed, vented storage tank or blowdown tank-with solid piping (no drip pan elbow, or other air gap). The storage tank should be located as close to the system as possible, but away from flammable surfaces. Overflow or high level protection should be considered. The capacity of the storage tank should consider the volume of fluid which may be relieved or sized in accordance with the heater manufacturer's recommendation. Storage tanks located outdoors shall be located such that water cannot collect in the vessel. When outdoor discharge is used,

the following should shall be considered for discharge piping hazards.

#### -at the point of discharge:

1) Both thermal and chemical reactions (personnel hazard);

2) Combustible materials (fire hazard);

3) Surface drains (pollution and fire hazard);

4) Loop seal or rain cap on the discharge (keep both air and water out of the system);

5) Drip leg near device (prevent liquid collection); and

64) Heat tracing for systems using high freeze point fluids along the discharge line (prevent blockage).

h) A condenser that will condense all the vapors discharged from the pressure relief valve may be used in lieu of piping the vapors to the atmosphere.

i) In order to minimize the loss by leakage of material through the pressure relief valve, a rupture disk may be installed between the pressure relief valve and the vaporizer, provided the following requirements are met:

1) The cross-sectional area of the connection to a vaporizer shall be not less than the required relief area of the rupture disk.

2) The maximum pressure of the range for which the disk is designed to rupture shall not exceed the opening pressure for which the pressure relief valve is set or the maximum allowable working pressure of the vessel.

3) The opening provided through the rupture disk, after breakage, shall be sufficient to permit a flow equal to the capacity of the attached valve, and there is no chance of interference with the proper functioning of the valve, but in no case shall this area be less than the inlet area of the valve.

4) The space between a rupture disk and the valve shall be provided with a pressure gage, try cock, free vent, or a suitable telltale indicator. This arrangement permits the detection of disk rupture or leakage.

<u>ji</u>) Pressure relief valve discharge capacity <u>for liquid service</u> shall be determined from the following equation:

 $\begin{array}{l} \hline W = \text{CKAP } \sqrt{(\text{M/T})} \\ \hline Where: \\ A = \text{discharge area of pressure relief value} \\ C = \text{constant for vapor that is a function of the ratio of specific heats k = cp/cv}. \\ \hline \textbf{Note: Where k is not known, k = 1.001.} \\ \hline \textbf{K} = \text{coefficient of discharge for the value design} \\ \hline \textbf{M} = \text{molecular weight} \end{array}$ 

 $\frac{P = (set \ pressure \times 1.03) + Atmosphere \ Pressure}{T = absolute \ temperature \ at \ inlet, \ ^{\circ}F + 460 \ (^{\circ}C + 273)}{W = flow \ of \ vapor}$ 

The required minimum pressure relief valve relieving capacity shall be determined from the following equation:

W = C x H x 0.75/h
 Where:
 C = maximum total weight or volume of fuel burned per hour, lb (kg) or ft3 (m3)
 H = heat of combustion of fuel, Btu/lb (J/kg) or Btu/ft3 (J/m3)
 h = latent heat of heat transfer fluid at relieving pressure, Btu/lb (J/kg)
 W = weight of organic fluid vapor generated per hour
 The sum of the pressure relief valve capacities marked on the valves shall be equal to or greater than W.

<u>For Liquid</u> <u>U.S. Customary Units</u> <u>W = 2,407KA  $\sqrt{(P - Pd)w}$ </u>

<u>SI Units</u> <u>W = 5.092 KA √(P - Pd)w</u>

Where.

 W = Liquid Capacity in lb/hr (kg/hr).

 A = Discharge Area of Pressure relief Valve, in² (mm²)

 K = coefficient of discharge for valve design

 P = (Set pressure + OP + Atmosphere pressure, psia (Mpa)

 OP = Overpressure required for Pressure Relief

 Valve to reach capacity specified in

 code of construction

 Pd = Pressure at discharge of valve, psia (Mpa)

 w = Specific weight of liquid at inlet condition

 lb/ft³ (kg/m³)

To convert lb/hr of water to gal/min, multiply the capacity in lb/hr by 1/500.

!!!!!!! ( SEE PART 1 PROPOSAL BEGINNING ON NEXT PAGE) !!!!!!!

#### PART 1

#### **S5.7 OVERPRESSURE PROTECTION**

#### **S5.7.1 GENERAL REQUIREMENTS**

Thermal fluid heaters shall be provided with overpressure protection in accordance with the code of construction.

#### S5.7.2 PRESSURE RELIEF DEVICES VALVES

Thermal fluid heaters shall be equipped with one or more pressure relief <u>devices valves</u> unless the option for overpressure protection by system design is utilized (when permitted by the original code of construction).

When pressure relief devices are used, the following shall apply:

a) Pressure relief valve(s) shall be of a totally enclosed type, and shall not have a lifting lever. A body drain is not required.

b) A lifting lever shall not be used in pressure relief valve(s). A body drain is not required.

b) Rupture disks may be installed upstream or downstream of the pressure relief valve(s) in accordance with the original code of construction.

c) Pressure relief valves and rupture disks shall be in accordance with the code of construction and designed for liquid, vapor, or combination service as required for the specific installation, service fluids, and overpressure conditions.

d) Cast iron fittings shall not be used

e) Copper and copper alloys shall not be used

df) The inlet connection to the valve shall be not less than NPS 1/2 (DN 15).

#### **S5.7.3 LOCATION**

Pressure relief <u>devices-valves</u> shall be connected to the heater in accordance with the original code of construction.

#### S5.7.4 CAPACITY

The pressure relief <u>device(s)valve(s)</u> shall have sufficient capacity to prevent the pressure vessel from exceeding the maximum pressure specified in the vessel code of construction.

#### **S5.7.5 SET PRESSURE**

a) When a single relief <u>device valve</u> is used, the set pressure marked on the device shall not exceed the maximum allowable working pressure.

b) When more than one pressure relief <u>device-valve</u> is provided to obtain the required capacity, only one pressure relief <u>device-valve</u> set pressure needs to be set at or below the maximum allowable working pressure. The set pressure of the additional relief <u>devices-valves</u> shall be such that the pressure cannot exceed the maximum pressure permitted by the code of construction.

#### **S5.7.6 INSTALLATION**

<u>Pressure relief valves and the associated discharge piping shall be installed in accordance with the heater Manufacturer's recommendations. The installation of the pressure relief valves required for Thermal Fluid Heaters shall include but not be limited to following requirements.</u>

a) <u>The pressure relief valve shall be provided with discharge piping</u>. When a discharge pipe is used, t<u>T</u>he cross-sectional area <u>of the discharge piping</u> shall not be less than the full area of the valve outlet. The size of the discharge lines shall be such that any pressure that may exist or develop will not reduce the relieving capacity or adversely affect the operation of the attached pressure vessel relief <u>devicesvalves</u>. Discharge piping shall be as short and straight as possible and arranged to avoid undue stress on the pressure relief <u>devicevalve</u>.

b) The pressure relief valve shall be connected to the pressure vessel in accordance with the original code of construction.

**b**<u>c</u>) The cross sectional area of the piping between the heater and the relief **device**-<u>valve</u> shall be sized either to avoid restricting the flow to the pressure relief **devices**-<u>valves</u> or made at least equal to the inlet area of the pressure relief **devices**-<u>valves</u> connected to it.

ed) When two or more required pressure relief devices valves are placed on one connection, the inlet cross-sectional area of this connection shall be sized either to avoid restricting the flow to the pressure relief devices valves or made at least equal to the combined inlet areas of the pressure relief devices valves connected to it.

<u>de</u>) Unless permitted by the code of construction, there shall be no intervening stop valve between the vessel and its pressure relief <u>device(s)valve(s)</u>, or between the pressure relief <u>device-valve</u> and the point of discharge.

ef) Pressure relief device valve discharges shall be arranged such that they are not a hazard to personnel or other equipment and, when necessary, lead to a safe location, such as a catchment tank, for the disposal of fluids being relieved.

fg) Discharge lines from pressure relief devices valves shall be designed to facilitate drainage. or be fitted with low point or valve body drains to prevent liquid from collecting in the discharge side of a pressure relief device. Drain piping shall discharge to a safe location for the disposal of the fluids being relieved. The possibility of solidification of fluid leakage into the discharge piping system shall be considered.

h) The pressure relief valve discharge shall be connected to a closed, vented storage tank with solid piping (no drip pan elbow or other air gap). The storage tank should be located as close to the system as possible, but away from flammable surfaces. Overflow or high level protection should be considered. The capacity of the storage tank should consider the volume of fluid which may be relieved or sized in accordance with the heater manufacturer's recommendation. Storage tanks located outdoors shall be located such that water cannot collect in the vessel.

The following shall be considered for discharge piping hazards.

1) Both thermal and chemical reactions (personnel hazard).

2) Combustible materials (fire hazard)

3) Surface drains (pollution and fire hazard)

4) Heat tracing for systems using high freeze point fluids (prevent blockage)

i) Pressure relief valve discharge capacity for liquid service shall be determined from the following equation:

For Liquid U.S. Customary Units  $W = 2,407KA \sqrt{(P - Pd)w}$ 

<u>SI Units</u> W = 5.092 KA √(P - Pd)w

Where.

 W = Liquid Capacity in lb/hr (kg/hr).

 A = Discharge Area of Pressure relief Valve, in² (mm²)

 K = coefficient of discharge for valve design

 P = (Set pressure + OP + Atmosphere pressure, psia (Mpa)

 OP = Overpressure required for Pressure Relief

 Valve to reach capacity specified in

 code of construction

 Pd = Pressure at discharge of valve, psia (Mpa)

 w = Specific weight of liquid at inlet condition

 lb/ft³ (kg/m³)

To convert lb/hr of water to gal/min, multiply the capacity in lb/hr by 1/500.

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PART 4

#### SUPPLEMENT 4 RECOMMENDED PROCEDURES FOR REPAIRING PRESSURE RELIEF VALVES S4.1 INTRODUCTIONSCOPE

This supplement contains recommended procedures for the repair, packaging, shipping and transportation of pressure relief valves. S4.2 contains recommended procedures for the repair of spring-loaded pressure relief valves., and S4.3

contains recommended procedures for the repair of pilot operated types of pressure relief valves. S4.4 contains linformation

on packaging, shipping and transportation. is included as S4.5.

a)-It is essential that the repair organization establish basic, specific procedures for the repair of pressure relief valves. The purpose of these recommended procedures is to provide the repair organization with guidelines for this important aspect of valve repair. It is realized that there are many types of valves and conditions under which they are repaired and, for this reason, the specific items in these recommended procedures may not apply, or they may be inadequate for each of those types or to the detailed repairs that may be required for each valve.

b) S4.2 contains recommended procedures for the repair of spring-loaded pressure relief valves, and S4.3

contains recommended procedures for the repair of pilot operated types of pressure relief valves. Information

on packaging, shipping and transportation is included as S4.5.

#### S4.2 SPRING-LOADED PRESSURE RELIEF VALVES

Prior to removal of a valve from a system for a repair or any disassembly, ensure that all sources of pressure

have been removed from the valve.

- a) Visual inspection as received
- 1) This information is to be recorded:
- a. Record user (customer) identification number;

b. Complete original PRV nameplate data, previous repair nameplate data, plus any important information received from customer;

c. Check external adjustment seals for warranty repair;

d. Check bonnet for venting on bellows type valves; and

e. Check appearance for any unusual damage, missing, or misapplied parts.

2) If sufficient damage or other unusual conditions are detected that may pose a safety risk during preliminary testing, then proceed directly to S4.2 c)

3) Valves that are to be repaired in place proceed to S4.2 c) unless preliminary testing has been authorized

by the owner.

b) Preliminary test as received

1) Information from the recommended preliminary performance test and subsequent disassembly and inspections will provide a basis for any repair interval change that should be necessary to ensure that the valve will function as intended.

 Determine set pressure or Cold Differential Test Pressure (CDTP) in accordance with manufacturer's recommendations and appropriate ASME Code Section. Do not allow test pressure to exceed 116% of set pressure unless otherwise specified by the owner. A minimum of three tests is usually required to obtain consistent results.

3) If results do not correlate with field performance, then steps to duplicate field conditions (fluid and temperature) may be necessary.

4) Record preliminary test results and test bench identification data.

c) Disassembly

1) Remove cap and lever assembly, if applicable.

2) Remove release nut assembly, if applicable.

3) Loosen jam nut on adjusting (compression) screw.

4) Record measurement and remove adjusting (compression) screw.

5) Remove bonnet or voke.

6) Remove spring and washers, and tag (identify) including upper and lower washers, as appropriate.

7) Remove spindle and disk assembly.

8) Remove ring pins.

9) Record measurement and remove adjusting rings, nozzle, and guide, as applicable.

d) Cleaning

1) Wire all small parts together and clean. (Caution: do not use a cleaning method that will damage the parts.)

2) Do not clean in a chemical solution except under acceptable circumstances.

3) Protect seating surfaces and nameplates prior to cleaning.

e) Inspection

1) Check spring for correct range, damage such as erosion, corrosion, cracking, or compression below free height.

2) Check nozzle for cracks (NDE as applicable) or unusual wear.

3) Check disk assembly for cracks (NDE as applicable) or unusual wear.

4) Check spindle for trueness, bearing areas, and thread condition.

5) Check guide for wear and galling.

6) Check adjusting ring(s) for worn threads and wear.

7) Check ring pins for bent or broken pin and thread condition.

8) Check bellows, if provided, for pinholes and corrosion.

9) Check flange gasket facings for wear and cuts.

f) Machining

Machine nozzle and disk as necessary to the manufacturer's critical dimension charts.

g) Lapping

1) Machine or hand lap disk and nozzle to be sure of flatness.

2) Lap bevel seats to a grey finish; then re-machine disk or plug to the manufacturer's critical dimension.

h) Bearing Points

Grind all bearing areas with grinding compound to make sure they are round and true.

i) Assembly

1) Install nozzle

2) Install lower ring and guide ring to the measurement from c) 9) above or to manufacturer's specifications.

3) Install guide

4) Install disc and holder

5) Install spindle

6) Install spring washers

7) Install bonnet

8) Install bonnet bolting

9) Install adjusting screw and lock nut to the measurement from c) 4) above,

10) Install release nut and lock nut, and cap and lever assembly, and

11) Document installation of replacement parts.

j) Testing

Test data shall be recorded. Testing will be done in accordance with manufacturer's recommendations and appropriate ASME Code section. To preclude unsafe and unstable valve operations or erroneous performance test results, it is recommended that low volume testing equipment (e.g., gas cylinders without

a test vessel, hand pumps, tubing) should be avoided.

k) Sealing

After final adjusting and acceptance by quality control inspection, all external adjustments shall be sealed with a safety seal providing a means of identification of the organization performing the repair. I) Nameplate

The repairer will place a repair nameplate on each repaired valve. The nameplate shall, as a minimum, meet the requirements of 4.7.1.

#### S4.3 PILOT OPERATED PRESSURE RELIEF VALVES

a) Visual Inspection as Received

1) This information is to be recorded:

a. Complete nameplate data, plus any other important information received from the customer;

b. User identification number, if applicable;

c. Seals on external adjustments (ensure seals are intact);

d. Identification on seal; and

e. Obvious damage and external condition including missing or misapplied parts.

b) Disassembly

1) Remove pilot and disassemble per manufacturer's maintenance instruction.

2) Disassemble main valve. Where lift adjustments are provided, do not remove the locking device or change the lift unless it is required as part of conversion.

3) Remove the nozzle if recommended by the manufacturer's maintenance instructions and/or when required as part of conversion.

c) Cleaning

1) Pilot — Components of pilot are small and must be handled carefully to prevent damage or loss. Clean parts and nameplates with solvents that will not affect the parent metal and/or polish with 500 grit paper.

2) Main Valve — Clean by appropriate means such as abrasive blast. Finishes of machined surfaces must not be affected. (Caution: Do not use a cleaning method that will damage the parts or nameplates.)

d) Inspection

1) Pilot

a. Check spring for damage such as corrosion, cracks, out of square ends, etc.

b. Inspect all parts for damage. Small burrs or scratches may be removed by polishing. Severely damaged parts should be replaced. (Internal components or pilots should not be repaired by machining as the functions of the pilot could easily be impaired.)

c. Check strainers and filters on inlet and outlet lines.

d. Replace all soft goods per manufacturer's recommendation.

2) Main Valve

a. Check nozzle seating surface for nicks. These can be removed by machining or lapping as required.

b. Check the piston and liner (or other moving member) for galling or excessive wear. The piston should move freely in the liner.

c. Replace soft goods or re-lap disk as required.

d. Where lift adjustments are provided, measure the lift per the manufacturer's specifications. e) Testing

Test data shall be recorded. Testing will be done in accordance with the manufacturer's recommendation and in accordance with the applicable ASME Code section. To preclude unsafe and unstable valve operations

or erroneous performance test results, it is recommended that low volume testing equipment (e.g., gas cylinders without a test vessel, hand pumps, tubing) should be avoided.

f) Sealing

After final adjustment and acceptance by quality control, all external adjustments shall be sealed by means assuring positive identification of the organization performing the repair.

g) Nameplate

The repairer will place a repair nameplate on each repaired valve. The nameplate, as a minimum, shall meet

the requirements of 4.7.1.

# S4.4 PACKAGING, SHIPPING AND TRANSPORTATION OF PRESSURE RELIEF DEVICES

a) The improper packaging, shipment, and transport of pressure relief devices can have detrimental effects on device operation. Pressure relief devices should be treated with the same precautions as instrumentation, with care taken to avoid rough handling or contamination prior to installation.
b) The following practices are recommended:

1) Valves should be securely fastened to pallets in the vertical position to avoid side loads on guiding surfaces except threaded and socket-weld valves up to NPS 2 (DN 50) may be securely packaged and cushioned during transport.

2) Valve inlet and outlet connection, drain connections, and bonnet vents should be protected during shipment and storage to avoid internal contamination of the valve. Ensure all covers and/or plugs are removed prior to installation.

3) The valve should not be picked up or carried using the lifting lever. Lifting levers should be wired or secured so they cannot be moved while the valve is being shipped or stored. These wires shall be removed before the valve is placed in service.

4) Pilot valve tubing should be protected during shipment and storage to avoid damage and/or breakage.

5) Valves for special services, including but not limited to oxygen, chlorine, and hydrogen peroxide, should be packaged in accordance with appropriate standards and/or owner procurement requirements.

#### **SUPPLEMENT 5**

#### RECOMMENDED GUIDE FOR THE DESIGN OF A TEST SYSTEM FOR PRESSURE RELIEF DEVICES IN COMPRESSIBLE FLUID SERVICE

#### S5.1 SCOPE

This supplement provides guidance for the design of a test system using compressible fluids (e.g., steam or

air/gas) and permits the determination of pressure relief valve set pressure and valve operating characteristics

such as blowdown.

The size of the test vessel needed depends on the size of the valve, its set pressure, the design of the test

system, and whether blowdown must be demonstrated. A repair organization may use the information provided

in this supplement to determine the minimum size test vessel needed so that the measured performance is characteristic of the valve and not the test system.

#### **S5.2 GENERAL**

a) The National Board administrative rules and procedures for the "VR" *Certificate of Authorization* and symbol stamp require that pressure relief valves, after repair, be tested in accordance with the manufacturer's

recommendations and the applicable ASME Code. The purpose of this testing is to provide reasonable assurance that valves will perform according to design when they are returned to service. b) It is recognized that a full evaluation of the performance of some pressure relief valve designs requires testing at maximum allowable overpressure. However, it is beyond the scope of this supplement to define test equipment or facilities for such testing.

c) Section 6 of this part provides a glossary, S5.3 describes typical test equipment, and S5.4 provides data

for estimating the size of test vessels required.

(Renumber all remaining sections)

#### SUPPLEMENT 6 PROCEDURES FOR REPAIRS TO ASME "NV" STAMPED PRESSURE RELIEF DEVICES

#### S6.1 INTRODUCTIONSCOPE

<u>This supplement provides procedures and requirements for repair of ASME</u> Code "NV" Class 1, 2, or 3 stamped pressure relief devices, which have been capacity certified by the

National Board, may be repaired provided the following requirements are met.

Item 19-1. Develop specific content and scope of annual field audits.

## 4.8.6.1 AUDIT REQUIREMENTS

## Initial Language

Upon issuance of a *Certificate of Authorization*, provided field repairs are performed, annual audits of the work carried out in the field shall be performed to ensure that the requirements of the Certificate Holder's quality system are met. The audit shall include, but not be limited to performance testing in accordance with 4.6 of valve(s) that were repaired in the field. The audits shall be documented.

## Proposed Language

Upon issuance of a *Certificate of Authorization*, provided field repairs are performed, annual audits of the work carried out in the field shall be performed <u>on an annual basis</u>. <u>The intent of these audits is to ensure work in the field is completed in accordance with</u> <u>the to ensure that the requirements of the Certificate Holder's quality system</u>. <u>are met.</u> <u>The scope and frequency of these audits shall be established in the quality system</u>. The audit shall include, but not be limited to: <u>performance testing in accordance with 4.6 of</u> <u>valve(s) that were repaired in the field</u>. The audits shall be documented.

- a) Performance testing in accordance with 4.6 of valve (s) that were repaired in the <u>field</u>
- b) Quality system requirements specific to field repair
- c) Certificate Holder's applicable ASME Code sections, VR special process (if applicable in the field), and test medias from the Certificate of Authorization.
- d) The audits shall be documented

#### 4.9 <u>COMPETENCY,</u> TRAINING AND QUALIFICATION OF PERSONNEL

# **4.9.1 COMPETENCY OF PERSONNEL**

<u>The repair organization shall establish the skills, knowledge, competencies, and method to evaluate competencies required for each position within the organization having direct effect on the quality of pressure relief repair performed in accordance with the Certificate of Authorization.</u>

# 4.9.24 CONTENTS OF TRAINING PROGRAM

- <u>a)</u> Applicable ASME Code and NBIC requirements;
- a)<u>b) Applicable NBIC requirements:</u>
- c) Individual responsibilities of each function described within the organization's quality system:
- d) Technical aspects for the applicable position held;
- e) Mechanical skills for the applicable position held;
- f) Special processes as applicable listed on the Certificate of Authorization.
- b) Responsibilities within the organization's quality system; and
- c) Knowledge of the technical aspects and mechanical skills for the applicable position held.

# 4.9.32 INITIAL EVALUATION AND ACCEPTANCE QUALIFICATION OF PERSONNEL

<u>The Each-repair organization shall complete an initial evaluation and acceptance of each individual's skills and competency prior to the individual being assigned to work without direct supervision. This evaluation and acceptance shall be documented.establish minimum qualification requirements for those positions within the organization as they directly relate to pressure relief valve repair. Each repair organization shall document the evaluation and acceptance of an individual's qualification for the applicable position.</u>

# 4.9.<u>4</u>3 ANNUAL <u>EVALUATION AND ACCEPTANCE REVIEW</u> OF <u>PERSONNEL</u> QUALIFICATION

The repair organization shall <u>complete an annual evaluation and acceptance of each</u> <u>individual's skills and competency to verify proficiency as well as compliance with the</u> <u>certificate Holder's quality system. This evaluation shall include training records,</u> <u>documented evidence of work performed and on-the-job observations to demonstrate</u> <u>competency.</u> <u>annually review the qualifications of repair personnel to verify proficiency as</u> <u>well as compliance with the Certificate Holder's quality system. This review shall include</u> <u>training records, docu- mented evidence of work performed, and when necessary,</u> <u>monitoring job performance. The review <u>evaluation</u> shall be\_documented.</u>